Project ID: FC339



# M2FCT: Million Mile Fuel Cell Truck Consortium

DOE Hydrogen Program 2021 Annual Merit Review and Peer Evaluation Meeting

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DOE AOP project award: WBS 1.5.0.402

JUNE 9, 2021

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# M2FCT Consortium - Overview & Relevance

#### Timeline

- Project start date: 10/01/2020
- Project end date: 09/30/2025

#### Budget

- FY20 project funding: \$10M
  - Sevent Planned \$ 1M external partners

  - 5-year consortium with yearly milestones & Go/No-Go

#### **Partners/Collaborations**

- DOE DE-FOA-0002044:
   GM, Nikola, Carnegie Mellon
- DOE DE-FOA-EE0009244:
  - 🏷 3 M, Lubrizol, Nikola, UT Knoxville
  - Scummins, Plug Power
- No-cost collaborations

FUEL CELL TRUCK

#### Heavy-Duty Transportation (2025)

- Durability: 25,000 hour lifetime
- 68% peak efficiency
- \$80/kW fuel cell system cost
- Overall Target: 2.5 kW/g<sub>PGM</sub> power (1.07 A/cn<sup>2</sup>) current density) at 0.7 V after 25,000 hour equivalent accelerated durability test

#### Heavy-Duty Transportation (2030)

- Durability: 30,000 hour lifetime
- 72% peak efficiency
- \$60/kW fuel cell system cost

### **Project Goals and Targets**

- Goal 1: Develop predictive models for cells and systems and exercise them to define realworld operation and component and assembly targets
- Goal 2: Develop materials that enable high efficiency and durable performance
- Goal 3: Evaluate rationally designed multicomponent MEAs comprised of tailored interfaces and components that exhibit transformational cell-level performance and efficiency
- Goal 4: Realize and interrogate ensembles of materials to elucidate and mitigate degradation
- Overall Target

2.5 kW/g<sub>PGM</sub> power (1.07 A/cm<sup>2</sup> current density) at 0.7 V after 25,000 hour -equivalent accelerated durability test



# Target Comparison between Light - and Heavy -Duty

Table 1. Technical Targets for Automotive-Scale (80 kWe netFuel Cell System Operating on Hydrogena

Characteristic	Units	Status	2020 Target	2025 Target	
Peak Energy Efficiency <sup>b</sup>	%	60 °	65	65	
Specific power	W/kg	659 <sup>d</sup>	650	900	
Cost <sup>f</sup>	\$/kWe	45 °	40	35	
Cold start-up time to 50% of rated power					ĺ
@ -20°C ambient temp	sec	20 f	30	30	Í
@ +20°C ambient temp	sec	<10 <sup>f</sup>	5	5	ĺ
Durability in automotive load cycle	hours	4130 <sup>g</sup>	5,000	8,000	
Unassisted start from <sup>h</sup>	°C	-30 <sup>i</sup>	-30	-30	

#### Table 1. Technical System Targets: Class 8 Long-Haul Tractor-Trailers (updated 10/31/19)

Characteristic	Unite	Targets for Class 8 Tractor-Trailers		
Characteristic	Units	Interim (2030)	Ultimate <sup>9</sup>	
Fuel Cell System Lifetime <sup>1,2</sup>	hours	25,000	30,000	
Fuel Cell System Cost <sup>1,3,4</sup>	\$/kW	80	60	
Fuel Cell Efficiency (peak)	%	68	72	
Hydrogen Fill Rate	kg H <sub>2</sub> /min	8	10	
Storage System Cycle Life <sup>5</sup>	cycles	5,000	5,000	
Pressurized Storage System Cycle Life <sup>6</sup>	cycles	11,000	11,000	
Hudrogon Storago Sustem Cost478	\$/kWh	9	8	
nyurogen storage system cost 45-	(\$/kg H <sub>2</sub> stored)	<mark>(</mark> 300)	(266)	

Condition	Traditional	M2FCT Focus
Operating temperature	60 - 80 ℃	~90 °C
Catalyst	Random alloy Pt <sub>90</sub> Co <sub>10</sub>	Tailored and ordered alloys, annealed Pt
Membrane	Ultra-thin, reinforced with mobile Ce	Stabilized, durable, high selectivity (H+ conductance/H <sub>2</sub> permeance)
Operating voltage	0.6 – 0.9 V	>0.7 V
Durability	5,000 hrs	25,000 hrs
Pressure	150 kPa	250 kPa
Catalyst loading	$0.15  g_{Pt}/cm^2$	$0.3 g_{Pt}/cm^2$

# Target Comparison between Light - and Heavy -Duty

Hydrogen Fuel Cell Diversity in Transportation



- Heavy-duty market is a critical market for reducing energy consumption and emissions
  - Medium- and heavy-duty trucks consume 25% of the total annual vehicle fuel use and produce 23% of the total CO<sub>2</sub> emissions in the US today
  - Annual freight truck miles traveled is projected to increase by 54% by 2050.
- Decades of development of cost-effective and durable polymer electrolyte membrane fuel cells needs to be leveraged to meet the increased efficiency and durability requirements of the HDV market

# M2FCT Approach

Million Mile Fuel Cell Truck (M2FCT) will tackle these challenges through a "team-ofteams" approach featuring main teams in analysis, durability, integration, and materials development. By coming together as sets of dynamic teams, the integrated consortium will provide rapid feedback, idea development, and information exchange, resulting in an effort that is more than the sum of its parts.





Approach

# M2FCT Approach

#### Integrated consortium

• An example of material and knowledge transfer for catalysts (Materials Development)





### **Organization Chart**



# **M2FCT Partners**



MILLION MILE







### M2FCT Kickoff Meeting Feedback

**Top technical priorities represented as Word Cloud** 

M2FCT Kickoff Meeting Feedback: Top technical priorities and Targets for M2FCT



Font sizes proportional to responses



Work, focus, and

specific funding

will change over

the years

# **M2FCT Initial Priorities**

#### 1. Analysis (\$1.325M)

- 1. Integrated system models
- 2. Cell models for analysis
- 3. Machine Learning/HPC/AI

#### 2. Materials development (\$0.900M)

- 1. Catalysts
- 2. Membranes and ionomers

#### 3. MEA Integration (\$2.395M)

- 1. Multicomponent integration studies
- 2. Benchmarking and baselining
- 3. Manufacturing

#### 4. MEA Durability (\$2.755M)

- 1. AST Development/cell correlation
- 2. Degradation mechanism discovery/mitigation

#### 5. Other (\$2.625M)

- 1. FOA support
- 2. Management & Communication
- 3. Discretionary funding for new concepts

#### Highest Emphasis year 1

#### Lowest Emphasis year 1

Medium Emphasis year 1 (Higher Benchmarking)

> High Emphasis year 1

For funding non-core labs and academia to fill identified portfolio gaps



### Year 1 Milestones

#### Establish consistent protocols and baselines between integration and durability that interface with analysis

Milestone Name/Description	Quarter	Status
Work statements finalized with industrial partners related to supporting HFTO-funded heavy-duty projects. (LBNL, LANL, ORNL, ANL, NREL)	Q1	
Voltage-loss breakdown methodology developed and utilized in analyzing modeling results for different operating temperatures and humidity. (LBNL, ANL)	Q2	
With DOE AST working group, propose new MEA durability ASTs incorporating relevant degradation mechanisms for catalyst, support, electrodes and membrane in a single AST. (LANL, ORNL, ANL, NREL)	Q2	
Acceptable transition metal loss from alloy catalysts (% of sulfonic acid sites in ionomer layer) defined with respect to electrode layer losses. (LBNL, LANL, ORNL, ANL, NREL)	Q3	
Establish benchmark performance, durability, and cost of a state-of-the-art MEA in relation to the DOE target of 2.5 kW/ $g_{PGM}$ power (1.07 A/cm <sup>2</sup> current density) at 0.7 V after 90,000 cycles of current catalyst AST. (LBNL, LANL, ORNL, ANL, NREL)	Q4	
High throughput, automated particle size/composition measurement demonstrated on MEA cross section encompassing >1000 particles. (ORNL)	Q3	
Deliver MEA for evaluation at NREL with cathode catalyst layer ionomer EW gradient (dual slot-die-coated on both membrane and GDL) with low EW at membrane interface and higher EW at MPL interface that exceeds 1.07 A/cm <sup>2</sup> at 0.7 V. (ORNL, NREL)	Q4	
Demonstration of concept using post-loading of metal oxides onto catalysts synthesized by LANL catalyst team, with catalyst ECSA of no less than 75% of baseline (carbon supported Pt based catalysts). (PNNL)	Q4	
Evaluate performance of intermetallic PtMN/C catalysts in comparison with benchmark performance and durability of a state-of-the-art MEA using commercial catalyst/support in relation to the DOE target of 2.5 kW/ $g_{PGM}$ power (1.07 A/cm <sup>2</sup> current density). (BNL, LANL, ANL, ORNL, NREL)	Q4	
FUEL CELL TRUCK		12

### Catalyst Materials Development Sub -Tasks

Q6 3/31/2022 Go/No-Go Can be extended to 24 (Q8) months as no -cost extension

Demonstrate  $\geq$  Statef-the-Art (Defined by Year 1Bench-Marking) at 0.8 V on hydrogen-air at 250 kPa, 100% RH, 80°C cell temperature after 90,000 catalyst AST cycles (or equivalent of M2FCT-developed AST) using an MEA with  $\leq 0.3 \text{ mg/cm}^2$  Total PGM loading



# **Communication & Outreach**

Vision: establish M2FCT as the premier research consortium not only at the research front but also for disseminating knowledge

- Outreach
  - & Company visits and interactions, international coordination
  - Sestablish the website and consortium as the go-to place for fuel cells especially for HDV, beyond mere data and publication output
  - Southly AST Working Group meetings
- In-reach
  - Internal newsletter, use uniform data procedures, storage, and trackers
  - Seekly technical meetings by technical area
  - Siweekly steering committee meetings
- Bring together the fundamentals of fuel-cell research and technology implications

# Inclusion, Diversity, Equity, Accountability

- Diverse group of researchers within the consortium
- Work with disadvantaged communities including HBCUs, HSIs, community colleges
  - Have various internships for students and targeted discretionary funding
  - Sexisting collaboration with NNSA to enhance STEM background & education
    - Including set-up of electrochemistry systems at HBCU's
    - Training, access to cuttingedge research, use of state-of-the-art facilities 0





Short Courses/Trainings



**On-site support** 

- Disadvantaged neighborhoods will be favorably impacted with improvements to long-haul trucking corridors and heavy-duty centers (*e.g.*, ports)\*
  - Screening of the transportation will greatly improve their local emissions and air and noise pollution

M2FCT Consortium	<b>Goal ①</b> Develop predictive models for cells and systems and exercise them to define real-world operation and component and assembly targets	<b>Goal 2</b> Develop materials that enable high efficiency and durable performance	<b>Goal ③</b> Evaluate rationally-designed MEAs comprised of tailored interfaces and components that exhibit transformational cell-level performance and efficiency	Goal ④ Realize and interrogate ensembles of materials to elucidate and mitigate degradation	Approach
Degradation Discovery AST Development	MEA AST Development	AST Testing & Component Degradation Mitigation	Synergistic Degradation Mitigation		
Materials	Catalysts	Catalyst Layer: Catalyst Ink + Ionomer	Components ⇒ MEA	MEA ⇒ HDV Fuel Cell	
Materials Baselining	Diffusion Media	Diffusion Media			
		lonomer-Membrane			
Integration & Analysis				2.5 kW/g <sub>PGM</sub> power (1.07 A/cm <sup>2</sup> current density at 0.7 V)	
Predictive System Models Define Real-world Operation	MEA Benchmarking Component Models	Component Down-selection Predictive Cell Models	MEA Manufacturing Cell Characterization	after 25,000 hour-equivalent accelerated durability test	
Establishing Benchmark Material Discovery	Material Synthesis and Development for Efficiency	Materials Selection, Optimization for Efficiency & Durability	Integrated Assembly Testing and Optimization	Cell Efficiency Final and Durability Target	
Year 1	Year 2	Year 3	Year 4	Year 5	



### M2FCT Approach Across Length and Timescale





### M2FCT Advanced Characterization Approach



Figure by A.Kusoglu



Nanostructure, Morphology, Interface

# M2FCT Advanced Computing Approach

Create a "Virtual Fuel Cell" digital twin

High performance computing for hifidelity and multiscale simulations





#### **Use HPC to provide data sets**



# Analyze and collect data sets of membrane properties for ML studies





### Analysis

#### Use cell models and system analysis to inform research



# Fuel Cell Systems for Medium and Heavy -Duty Trucks



#### **Salient Features**

- 275 kW net (35-kWh ESS) at EOL
- Multiple stacks: 4
- Electrodes
- Cathode: a-Pt/C, 0.25  $mg_{Pt}/cm^2$ , 50 wt% Pt Anode: Pt/C w IrO<sub>2</sub> (TBD), 0.05  $mg_{Pt}/cm^2$
- Membrane: 14 mm, chemically stabilized, mechanically reinforced
- Single air system with expander
- Single anode system with recirculation blower
- Cathode humidifier: No (TBD)
- Rated power conditions at EOL: 2.5 atm, 87-95°C, 660-700 mV
- Control valves for startup and shutdown, cold start and OCV

# Simulated Heavy -Duty Fuel Cell Operation (Class 8 Truck)



**Operating Times and Conditions for HDV** 

Rated power conditions:

✤ 275-kW FCS

- ♦ 0.7 V cell voltage
- ♦ 90°C coolant exit temperature\*
- 4 2.5 atm inlet pressure

\*only achieved under sustained high power hill climb

#### **FCS-HDV Duty Cycle Simulation**

- Power demand from Autonomie<sup>1</sup> for three HDV vocations on EPA fuel economy cycles
- Conducted drive cycle simulations for fuel cell dominant power train with battery for regenerative breaking, hill climb, and power demand exceeding 275 kW<sub>e</sub>
- 20-kW<sub>e</sub> FCS idle power clips cell voltage to 880 mV
- OCV controlled to 760 mV by shutting off H<sub>2</sub> supply when FCS power demand is below 20 kW<sub>e</sub>
- High temperatures limited by operating fan when coolant exit T exceeds the set target (65°C)
- Next steps: Harmonize duty cycles with the 21<sup>st</sup> Century Truck Partnership

# FC System Energy Consumption at Different Power Levels

Key to improving fuel economy of Class-8 vehicles is to focus on performance at rated power

- Slightly more H<sub>2</sub> is consumed near rated power in regionals than in multi-purpose and urban vocations
  - $H_2$  consumption decreases at lower power
  - ✤ Peak occurs at FCS idle power



- 50% of H<sub>2</sub> is consumed above 160 200 kWe FCS power
- 75% of H<sub>2</sub> is consumed above 150 kWe for regionals, 125 kWe for multi-purpose, and 100 kWe for urban



#### **FCS-HDV Degradation Adjusted Stack Size**

Lifetime defined by ECSA loss as marker of aging (275  $\rm kW_e$  at EOL)



#### 90-95°C coolant



FUEL CELL TRUCK

- Stack size defined by efficiency target
   Stack coolant exit temperature at peak power
- Stack active area defined for various catalyst degradation for 700 mV (EOL cell voltage)

#### **Modeled Electrode Degradation Mechanisms**

- $\backsim$  ECSA loss due to Pt dissolution and growth in particle size
- ✤ Degradation in ORR kinetics
- ✤ Increase in oxygen transport resistance
- ♦ Change in Pt accessibility
- Relaxing EOL cell voltage to 660 mV decreases the initial stack active area by 10-15%
  - Stack coolant exit temperature at peak power, ~ 50°C higher

2.5 atm, 1.5 SR(c), 0.3 mg/cmPt, a-Pt/HSC cathode catalyst

# Reaching Peak Efficiency Targets: Catalyst Activity and Operating Conditions

- Calculated cell voltages required to reach the target peak efficiencies
  - 4 860 mV for 63% efficiency
  - ✤ Interim: 910 mV for 68% efficiency
  - ✤ Ultimate: 956 mV for 72% efficiency
- Determine catalyst mass activities required to reach the target peak efficiencies
  - $\bigcirc$  0.3 A/mg-Pt for a-Pt/C with 0.25 mg-Pt/cm<sup>2</sup> loading
  - ✤ Interim: 1.5 A/mg-Pt (5 X status)
  - Ultimate: 7.5 A/mg-Pt (25X status)

Peak Efficiency Metrics	Status	Interim	Ultimate
CEM Turndown	10	20	20
Parasitic Losses, %	5	3.4	3.3
Current Efficiency, %	94.7	95.7	96.8
BOL Peak Efficiency, %	63.2	68.5	72.3
EOL Peak Efficiency, %	59.2	65.7	70.3
BOL Cell Voltage, mV	860	910	956
EOL Cell Voltage, mV	809	878	933
BOL Current Density, mA/cm <sup>2</sup>	53.4	67.5	91.4
EOL Current Density, mA/cm <sup>2</sup>	51.2	63.2	84.5

$$\eta_s = (1-\zeta)\eta_i\left(\frac{E}{\Delta H/F}\right)$$

- $\eta_s$ : Peak efficiency;
- $\boldsymbol{\zeta}$ : Parasitic loss;
- $\eta_i$ : Current efficiency;
- *E*: Cell voltage;
- $\Delta H$ : Lower heating value

\*T = 65°C Ambient Outlet Pressure

#### Methods to Reach Target Efficiencies

- Increase catalyst MA (new catalysts)
- Low- $\lambda$  content membranes (new ionomers)
- Increase OCV (decrease H<sub>2</sub>/O<sub>2</sub> cross-over)
- Increase kinetics (increase operating temp.)





# Parameter sensitivity analysis from physics -based model

• How sensitive is cell output  $f_i$  to input

$$\kappa_{ij} = \frac{\partial \log f_i(x)}{\partial \log x_j} = \frac{1}{\delta} \left( \frac{f_i(\mathbf{x} + \delta x_j \mathbf{e}_j)}{f_i(\mathbf{x})} - 1 \right)$$

- Model Inputs
  - Solutions of the second second
- Cell condition variables as outputs
- Multiple operating conditions
- Heatmap shows log of the sensitivity magnitude
  - Red is negative sensitivity and blue is positive
- Crucial parameters at dry conditions (80°C, 40% RH, air)
  - Solution Cathode kinetics and membrane



- $\kappa_L$ : Membrane conductivity in liquid
  - $\kappa_V$ : Membrane conductivity in vapor
- $\lambda$ : Membrane water uptake
- $\xi$ : Electro-osmotic coefficient
- $\alpha$ : Water diffusivity
- $A_v$ : Catalyst specific area (anode/cathode)
- $i_0, \alpha_a, \alpha_c$ : Exchange current, transfer coefficients
- $r_{agg}, \delta_{agg}$ : Radius of agglomerate and film thickness
- $D_{O_2,m}$ : Oxygen diffusivity in ionomer
- D<sub>ij,bulk</sub> : Bulk diffusivity
- $\epsilon_G$ : Gas volume fraction
- S<sub>L</sub>: Liquid saturation
- $\tau_G$ : Tortuosity
- $k_0$ : Absolute permeability
- k<sub>r</sub>: Relative permeability
- $k_T^{eff}$ : Effective thermal conductivity  $\sigma^{eff}$ : Effective electronic conductivity

# Parameter sensitivity analysis from physics -based model

- Crucial parameters at 80°C, 80% RH, air
   Cathode kinetics parameters: slow ORR
   Mancherene hadrations descendents
  - Membrane hydration: dry membrane
    GDL transport: low O<sub>2</sub> partial pressure
- $f_i$  sensitivity to  $x_i$ ,  $\log_{10}(\kappa_{ii} > 0.1)$ 0.76 Anode kinetics Cathode kinetics -0.24 Gas transport { Thermal properties -1.25 Ionomer properties -0.24 Operating conditions  $\langle$ RH Cell geometry { 0.76

80C, 80% RH, air

- $\kappa_L$ : Membrane conductivity in liquid  $\kappa_V$ : Membrane conductivity in vapor  $\lambda$ : Membrane water uptake  $\xi$ : Electro-osmotic coefficient  $\alpha$ : Water diffusivity  $A_{v}$ : Catalyst specific area (anode/cathode)  $i_0, \alpha_a, \alpha_c$ : Exchange current, transfer coefficients  $r_{aaa}, \delta_{aaa}$ : Radius of agglomerate and film thickness  $D_{O_2,m}$ : Oxygen diffusivity in ionomer *D*<sub>*ii*,*bulk*</sub> : Bulk diffusivity  $\epsilon_{c}$ : Gas volume fraction  $S_{I}$ : Liquid saturation  $\tau_G$ : Tortuosity  $k_0$ : Absolute permeability  $k_r$ : Relative permeability  $k_{T}^{eff}$ : Effective thermal conductivity  $\sigma^{eff}$ : Effective electronic conductivity
- Crucial parameters at 80°C, 80% RH, 5% O<sub>2</sub>
   Cathode kinetics parameters: slow ORR
   GDL, MPL, CL transport properties: O<sub>2</sub> limited cell





# Durability

#### Understanding, evaluating, and mitigating durability concerns with materials-based solutions



# **ASTWG (Working Group) Charter**

- Recommend protocols and targets related to heavy duty application of fuel cells
- ASTs for use in M2FCT for target evaluations (targets are End-of-Life)
- ASTs to be developed
  - Catalyst
  - ♦ Catalyst support
  - 🏷 Membrane chemical
  - ✤ Membrane combined chemical mechanical
  - ♦ SD/SU
  - Anode  $H_2$  starvation
  - Step MEA drive-cycle

#### Participants

ANL Ballard Carnegie Mellon DOE GM LANL LBNL Nikola NREL ORNL Cummins Plug Power Chemours

#### Define the 25,000 hour equivalent AST in the M2FCT 2025 Target

2.5 kW/g<sub>PGM</sub> power (1.07 A/cm<sup>2</sup> current density) at 0.7 V after 25,000 hour -equivalent accelerated durability test

# **ASTWG: Catalyst Durability Protocol**

- Develop H<sub>2</sub>/Air tests to measure degradation rates under accelerated conditions
- Operate cell @90°C to accelerate all degradation mechanisms for the longer life time
  - Potential cycling between 0.65V and 0.925V under 100%RH to accelerate catalyst degradation
  - Introduce RH cycling and dry operation to accelerate membrane degradation
- Degradation rates under accelerated conditions will be compared with rates at typical LDV and HDV operating conditions to determine duration of AST to yield 25,000 hours equivalent durability

Pt			PtCo		
Hours	A/mg-Pt	Hou	urs A/mg-P	't	
0	0.31	0	0.47		
50	0.23	5(	0 0.33		
100	0.21	10	0.23		
200	0.17	20	0.18		
300	0.13	30	0.14		



- PtCo has mass activity =  $0.47 \text{ A/mg}_{Pt}$  at BOL while Pt =  $0.31 \text{ A/mg}_{Pt}$
- At 300 hours both have almost the same mass activity of 0.135 A/mg<sub>Pt</sub>

Current plan: Extend out catalyst AST to 90,000 cycles from 30,000 cycles



0.5

# **Time-resolved Measurement of Catalyst Dissolution**

- Dissolution of both Pt and alloying metal measured in aqueous electrolyte during potential control
- Sensitivity at <10 ppt</p>
- Dissolution can be correlated with oxidation state of catalyst using cyclic voltammetry and/or in situ X-ray absorption spectroscopy
- Catalyst degradation mechanisms analyzed using thermodynamic and kinetic modeling
- New cell developed to allow deaeration of electrolyte enabling determination of the effect of dissolved oxygen

On-line ICP-MS detection of Pt and Co used to determine regions of voltage stability and to elucidate degradation mechanisms





XAFS Scan No.

7 8 9 10 11 12 13 14

Correlation of Pt and Co loss

with Oxide Formation and

Reduction



0.05

0.00

0.9

08

0.7 (N vs RHE)

0.4 ш

0.3

0.2

0 1 2 3 4 5 6



BOL Pt/Co: 88/12

EOL Pt/Co: 89/11

# Identical Location (IL) -STEM Capability



b) 20 nm

Morphology and composition changes observed before and after cycling catalyst on Au TEM grid in aqueous three electrode cell
 Driving primarily particle coalescence degradation mechanism (Pt/C TKK)
 Little Ostwald ripening observed in IL-STEM tests, in stark contrast to MEA testing of PtCo cathodes



# **Catalyst Durability Case Study: Modeling**

Differential cell performance at BOL and after 90k 0.6-0.95 V AST cycles, 80°C, 100% RH, 0.2 mg/cm<sup>2</sup> cat loading



- For high stoics at BOL, d-PtCo/C is superior to a-Pt/C and Pt/C at all current densities
- ECSA loss similar for d-PtCo/C and a-Pt/C but much higher for Pt/C
- Performance loss at high current densities after 90k cycles: d-PtCo/C > Pt/C > a-Pt/C
- Based on differential cell data, all three catalyst systems are potential candidates
- M2FCT target is for integral cell performance at 0.7 V after 25,000 h
   \$\$ 2.5 kW/g<sub>PGM</sub> and 750 mW/cm<sup>2</sup> at 0.7 V after 25,000 h, 2.5 atm, 87°C, 2/1.5 anode/cathode stoichiometry

# Catalyst Durability Case Study: Effect of aging

#### **ORR Kinetics**

- Fresh Pt/C and a-Pt/C have comparable specific  $i_{0r}$  (exchange current density) but Pt/C has higher kinetic activity on g-Pt basis
- Pt/C and a-Pt/C exhibit similar aging of  $i_{0r}$
- d-PtCo/C has higher  $i_{0r}$  at BOL but decreases with aging



#### **O**<sub>2</sub> Transport Resistance

- Slope  $R_{O2}$  and intercept (Micropore resistance  $(R_c)$ ) change with aging
- Pt/C and a-Pt/C:  $R_{O2}$  decreases with aging
  - Redistribution of Pt from pores to surface
- d-PtCo/C:  $R_{O2}$  slightly increases w/aging; Co dissolution and poisoning



# **GDLs for Cation Transport Suppression**

- Cations are present in PFSAs as radical scavengers (Ce and Mn), contaminants (Ca), byproducts of catalyst dissolution (Co and Ni), and from corrosion of BOP components (Fe)
  - Fe transport through GDL (from BPP corrosion or BOP components) problematic for membrane durability

#### Studied GDL/MPL morphology effect on cation transport



MPLs with cracks and hydrophilic GDLs show enhanced cation transport

#### **GDL** modification to suppress the Cation transport rates



Addition of Pseudo MPL Addition of hydrophobic layer

- Novel GDLs suppress cation transport from the flow field
  - Smaller Fe<sup>2+</sup>/Fe<sup>3+</sup> redox couple post-flowfield injection of Fe
  - Solution AST corrodes the 29BC and H23C8 MPL significantly and increases the Fe transport rates

#### Flowfield injection of Fe to study cation transport

#### Fe<sup>2+</sup>/Fe<sup>3+</sup> redox couple obtained from CV



- Subtracting the after curve from the before curve to obtain the Fe redox curve
- Peak current used to calculate the Fe loading in the catalyst layer
- Modified 29BC shows significant suppression of Fe transport even after AST

# Integration

#### Glean fundamental information pertinent to the integration of known and novel materials




## **Baselining Roll -to-Roll MEA Performance**



CELL TRUCK

Loc	ation	50 cm <sup>2</sup>	5 cm <sup>2</sup>
L	BNL	2	3
(	GM	2	3
L	ANL	2	3
A	NL	0	2-3
N	IIST	2	
C	MU	2	2
Ni	kola	2	
N	REL	4	3-4





## **Catalyst -Layer Formation**

High-water-concentration dispersions lead to fewer secondary aggregates



Synergistic conclusions from fundamental and in-situ investigations

# **Catalyst -Layer Formation : PFSAFormation**

High-water-concentration

dispersions = more regular arrangement of primary aggregates, fewer secondary aggregates

 Formation of crystalline domains occurs first



Analyzed dispersion structure with Grazing Incidence Small Angle X-Ray Scattering



## **Catalyst -Layer Formation : PFSAFormation**

### **Thin-Films: Dispersion-Cast**

 Annealed films: swelling decreases with increasing dispersion water fraction
 Software Formation behavior persists after annealing

### **Membranes: Dispersion-Cast**

- Ionic conductivity increases with dispersion water content
  - Swelling is less sensitive to concentration
  - Impacts the connectivity of conducting domains



# **Catalyst -Layer Formation : Ink Interactions**

Pt/PFSA interactions are similar to C/PFSA interactions, and governed by a similar mechanism





- ITC conducted in 100% water, with Vulcan or Pt black nanoparticles
- ITC trends agree with QCM data (strongest adsorption for 3M 825 for carbon, weaker binding with increasing EW on Pt)
- On both platinum and hydrophobic surfaces, binding is a function of EW, and increases as dispersion water content increases

### **Binding Mechanism**



 Binding is entropically dominated on both surfaces during formation: hydrophobic interactions

## **Catalyst -Layer Formation : Ink Interactions**

- Carbon/Pt surface areas influence ink interactions and CL performance
  - High I:C results in catalyst layer changes due to excess ionomer impacting ink properties
    - Greater than monolayer type coverage
    - Function of Pt weight percent due to interactions





46wt% CL – agglomerated structure

### Electrode Structure - Performance





### **Electrode Structure – Crack Mitigation**

#### **Ink Formulation**

Catalyst wt %	I/C	H <sub>2</sub> O wt%
3.5	1.00	66 or 17

### **Additive Details**



Poly (vinyl alcohol) – PVA Molecular Weight: 89-98k

Poly (methyl methacrylate) – PMMA Molecular Weight: 120k



Goal of this study: Utilize additives as means to mitigate catalyst-layer crack formation

Approach: Insert polymeric additives before the final mixing stage (relative to ionomer mass)

Micrograph (500x) Comparison Utilizing Our Crack Detection Algorithm



Alcohol-rich control 0.278 – 0.308 mg Pt/cm<sup>2</sup>



Water-rich w/ 5% PVA 0.273 – 0.280 mg Pt/cm<sup>2</sup>



Alcohol-rich w/ 5% PMMA 0.262 – 0.300 mg Pt/cm<sup>2</sup>



#### Crack % Reduction







## **Integrating Novel Materials**



- Ordered inter-metallic PtCo/Vu developed within M2FCT (Stamenkovic)
- Sulfonated polymerized ionic liquid block co-polymers (SPILBCP) from Drexel and Texas A&M University

Integration methods based on Neyerlin and coworkers ACS Energy Lett. 5, 1726-1731 (2020)

 30% increase in mass activity translates to improved efficiency throughout the entire voltage range

- Anode: Pt/HSC (TKK, 46.8 wt%), L = 0.05 mg<sub>Pt</sub>/cm<sup>2</sup>, 7w3N, I/C = 0.9
- Cathode: PtCo/V (UCI, 13.1/vt%), L = 0.1 mg<sub>Pt</sub>/cm<sup>2</sup>, 6w4AcN, I/C = 0.6Nafion:C or 0.3SPILBCP:C+0.3Nafion:C
- 5 cm<sup>2</sup>, differential cell

### **Materials Development**

### Synthesizing novel stable and efficient materials for heavy-duty applications



- Pt intermetallics on nitrogendoped graphitic supports
- Addition of metal oxide (AOx) around Pt and PtM NPs on carbon to stabilize them
- Nitriding of Pt intermetallics
- Control of particle shape, intraparticle composition and structure to inhibit metal dissolution
- Control particle-ionomer interface

Incorporation and testing in MEAs for performance and durability



## Structure Engineering for Particles and Supports



NPGC support possesses an intermediate surface area and porosity compared with the Vulcan carbon support and High -surface area carbon (HSC) support, which renders the catalyst balanced activity, power density, and stability



## **Oxide Nanoparticles for Stability**

- Particle size of 1 to 5 nm can be precisely controlled by using RME method with
- High yield of AOx (through RME) offers the possibility of synthesis scale-up
- Deposition sequence is the key parameter to affect ECSA
  - AOx slightly decreases ECSA and ORR activity – new synthesis to mitigate it



Pt/C WO<sub>3</sub>/Pt/C ZrO<sub>2</sub>/Pt/C



## **Intermetallic Synthesis & Characterization**

• ORR performance of Intermetallic PtNiN/KB (RDE)

Cycle #	MA (A/mg)	ECSA (m²/g)	SA (mA/cm <sup>2</sup> )	<i>E</i> <sub>1/2</sub> (mV)
ОК	1.83	62.6	2.92	935
30K	1.33 (-27%)	60.3 (-3.7%)	2.21 (-24%)	924 (-11)

- MEA: MA (0.49 A/mg), MA loss after 30K (-35%), and current density at 0.8V (348 mA/cm2) exceeded the DOE 2020 LDV targets
- High-pressure nitriding (HPN) Strategies to further improve the ORR performance
   Enhanced activity of shape-controlled PtM catalysts by HPN without changing the size and morphology

#### N-doped Intermetallic PtNiN/KB Initial • BOL (0 k) Current density (mA cm<sup>-2</sup>) -- After 10k cycles - EOL (30 k) — After 20k cycles After 30k cycles Voltage (V) Int-PtNiN/KB 0.6 MEA at LANL RDE 100 % RH, 150 kPa 0.4 0.0 0.5 1.0 1.5 0.4 0.6 0.8 1.0 Current density (A cm<sup>-2</sup>) Potential (V vs RHE) Pressure controller

#### Up to 10 MPa 00 (1500 psi) & sample Solenoic 1000°C Water furnace valve cooler acid solution scrubber 5% NH<sub>3</sub>, bal N<sub>2</sub> pressure cylinder transducer max temp 1000°



### **Intra-particle Composition & Structure**

- Dissolution of Pt and Co inhibited by formation of ordered intermetallic structure
- Dissolution of Pt inhibited by an Au core underlying Pt skin
- ECSA and MA loss only 20% after 30K AST cycles for PtAu







Γ<sub>Co</sub> (ng cm<sub>geo</sub><sup>-2</sup>)

<sup>1</sup>Pt (ng cm<sub>geo</sub><sup>-2</sup>)

0.01

1.0

1.1

E (V vs. RHE)

1.2

### Au Core eliminated Pt dissolution up to 1.2V vs. RHE





 P.P. Lopes, D. Li, H. Lv, C. Wang, D. Tripkovic, R. Schimmenti, H. Daimon, Y. Kang, J. Snyder, N. Becknell, K.L. More, D. Strmcnik, N.M. Markovic, M. Mavrikakis, & V.R. Stamenkovic, Nature Materials 19, 1207-1214 (2020).

## **Ionomer Synthesis**

 Development of novel perfluoro chemistries for membranes and ionomers with exceptionally high conductivity, targeting improved selectivity and catalyst/ionomer interactions





 TGA results indicated the composite polymer contained 38% Ce(NO<sub>3</sub>)<sub>3</sub> (1:1 ratio: 42%)



## **Collaborations: M2FCT Partners**



2020 H2@Scale FOA HD Membrane Projects Image: Scale FOA Membrane Projects Image: Scale FOA Image: Scale FOA



 Virtual meetings held between M2FCT steering committee and 7 MEA/Membrane projects

**Status of Interactions** 

- Updates/introductions to projects
- $\bigcirc$  Discussion 2021FOA support needs
- All nine FOA projects presented at M2FCT kickoff meeting
  - $\$  Cummins and Plug Power manufacturing projects interested in testing M2FCT MEAs
- NDAs executed with GM, Nikola, and CMU
  - ♥ NDAs in progress with membrane and manufacturing projects
- FOA project folders hosted on M2FCT google drive
  - ♥ Presentations with statements of work.
- Searchable PI and Capabilities list being generated for M2FCT website
- Quarterly meetings to be held between FOA Coordination Officer and FOA PIs
  - $\clubsuit$  Discuss current FOA support efforts and challenges
  - Seffort captured in quarterly reports

Also have collaborations through the discretionary funding

### **Collaborations: Non-FOA activities**

Entity	Scope of collaboration	Entity	Scope of collaboration
AvCarb	R2R gas diffusion electrode fabrication	SUNY Buffalo	Catalyst carbon supports
3M	lonomer materials and discussions for ionomer studies	Advent	Membrane development
Drexel University	Sulfonated ionic liquid block co-polymer	U. South Carolina	Catalyst development
N.E. Chemcat	Development of Pt core-shell catalysts	U. Louisville	Electrode structures
Toyota North America	Development of catalysts for light-duty vehicles	Georgia Tech	Lattice Boltzmann modeling
IUPUI	Development of PBI-modified carbon	Virginia Tech	Membrane characterization
Umicore	Provide tailored MEAs	RPI	Membrane development
U Delaware	Membrane durability with radical stabilization	Texas A&M University	Sulfonated ionic liquid block co- polymer
Robert Bosch	Voltage loss analysis and modeling discussions	Toyota Research Institute	Machine learning for membrane design



## **Future Work**

- M2FCT consortium aimed at delivering MEAs and components that meet 2.5 kW/gPGMpower (1.07 A/cm<sup>2</sup> current density) at 0.7 V
  - ✤ Targets are end-of-life performance
  - Sreater efficiency (68-72%)
  - High durability (1,000,000 miles; 25,000-30,000 hrs)
  - ♦ Material down-selects ~ year 3
    - Catalyst areas Go/No-Go at Q6

### Analysis

- Refine models, characterization, and diagnostics for heavy-duty operating conditions
- Define operating conditions efficiency and durability trade-offs
- Coordinate and harmonize truck platforms and duty cycles
- Compare systems with different ratios of fuel cell power and battery energy storage
- Sensitivity of performance, durability and cost to cell voltage target at EOL
- ✤ Incorporate membrane durability in system analysis

### Machine learning / Data analysis

Correlations of metadata for material and integration studies

### High-Performance Computing

- Unsteady FCS simulations on truck drive cycles
- Sectore and agglomerate structure
- Upscaling physics-based micro- and nano-scale models to cell models and optimization

### Durability

- Develop refined ASTs for lifetime prediction with heavy-duty materials and operating conditions
  - Refine existing LDV ASTs
  - Develop new ASTs/protocols specific for HDV
- Propose new protocols in collaboration with ASTWG by end of FY21
- Selectrode stability
- ⅍ Membrane and ionomer durability with additives
- High-temperature operating time effect on durability
  - Membrane
  - Catalyst
- Understand long-term durability effects on other components (GDL, contamination, reversible degradation, carbon corrosion at operating potentials)



## **Future Work**

### Integration

- Solution Solution & Baseline Solution
  - Establish benchmark performance and cost of state of-art MEA
- Incorporate advance catalyst ink understanding into R2R manufacturing
- Integrate newly developed materials into optimized MEA structures
  - Membranes
  - lonomers
  - Catalysts
  - Catalyst supports
  - GDLs
- Catalyst layer studies
  - Understand cation migration effects on catalyst layer performance
  - Catalyst layer porosity
  - Catalyst ink to structure formation models
- Stransport Properties (Gas phase, water, cations)
  - Catalyst Layer
  - GDL

### Material Development

- Catalysts & Catalyst supports
  - Pt-Co Intermetallics
  - Metal oxide-metal-carbon junction to stabilize PtM NPs catalysts
  - Nitrogen-Doped PtMN Catalysts and Supports
  - Tailored Ptnanomaterials, supports, and interfaces
- Membranes & Ionomers
  - High-conductivity Novel Perfluorinated Ionomers
  - Low Molecular WeightOligomeric Electrode and Membrane lonomers
  - Composite PFSA Membranes and Ionomer EW and Side-Chain Chemistry
- ♦ Other components (GDLs, Bipolar plates...)
- **Material and characterization studies**

Planned activities include discretionary funding for additional collaborators on identified gaps and needs



## Summary

- Relevance/Objective:
  - Solution by the second descent of the second durability of fuel-cell components and assemblies
  - Semphasis to support heavy-duty transportation applications
- Approach:
  - Synergistic combination of modeling and experiments to develop materials, optimize component properties, behavior and phenomena
    - o Analysis
    - Durability
    - Materials development
    - Integration
- Technical Accomplishments:
  - Solution Soluti Solution Solution Solution Solution Solution Solution S
  - Surability measurements at projected heavy-duty loadings
    - Development of heavy-duty related ASTs
  - State St
    - o Ink composition-solvent studies, cell testing, impact of fabrication, membrane and ionomer characterization, cell and CL modelign
  - Material Developments
    - Higher mass activity/durable catalyst
    - Advanced ionomers and membranes for durable hightemperature operations
- Future Work:
  - Emphasis on efficiency and durability
  - Solution to develop the knowledge base to improve catalyst layer structures and component integration



### Who is M2FCT? National Lab Contributors



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## Acknowledgements

DOE EERE Hydrogen and Fuel Cell Technologies Office

**Technology Managers:** 

**Greg Kleen, Dimitrios Papageorgopoulos** 



**U.S. DEPARTMENT OF ENERGY** 

http://millionmilefuelcelltruck.org



### **User Facilities**

DOE Office of Science: SLAC, LBNL-Advanced Light Source, LBNL-Molecular Foundry, ANL-Advanced Photon Source, LBNL-Molecular Foundry, ORNL-Center for Nanophase Materials Sciences, ANL-Center for Nanostructured Materials, NIST: BT-2



# Technical Backup and Additional Information



## **Technology Transfer Activities**

- Copyright of microelectrode drawings
  R&D 100 award
- Engaging with various stakeholders and OEMs including FOA projects and others as noted
- Publications, presentations, discussions
- Outreach through website development



### **Publications**

- Katzenberg, Adlai, Debdyuti Mukherjee, Peter J Dudenas, Yoshiyuki Okamoto, Ahmet Kusoglu, and Miguel A Modestino. "Dynamic Emergence of Nanostructure and Transport Properties in Perfluorinated Sulfonic Acid Ionomers." *Macromolecules* 53.19 (2020) 8519-8528.
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### **Progress toward DOE Targets or Milestones**

### M2FCT 2025 Target

2.5 kW/ $g_{PGM}$  power (1.07 A/cm<sup>2</sup> current density) at 0.7 V after 25,000 hour -equivalent accelerated durability test

• Existing baseline efforts with new materials and also development of AST and test protocols mean that it is too early yet to judge where we are at in terms of this metric



### FCS for Medium and Heavy-Duty Trucks: Air Management

	Units	High	Medium	Low
		(H)	(M)	(L)
Compressor Efficiency	%	75	72	70
Expander Efficiency	%	80	75	70
Combined Motor & Motor Controller Efficiency (M&MC)	%	90	85	80
Pressure Drop: Compressor Outlet to Expender Inlet ( $\Delta P$ )	psi	5	5	5



- Feasible to have a single air system with <27 kW<sub>e</sub> parasitic power if H or M component efficiencies can be achieved
- Recommended performance targets to DOE for FOA on air management system for HD trucks

## **FCS Heat Rejection on Hill Climb**

Modeled system equivalent to radiator fan for 450-hp diesel engine, 52°C air-to-boil temperature



### **Study Conclusions**

Study parameters: Hill climb at 30 mph, 6% grade, 20-min duration, 25°C ambient temperature

- 1. Largest FCS for which waste heat can be rejected using radiators in a 450-hp diesel trucks: 275  $\rm kW_{e}$  net
- 2. Smallest battery operated in charge depleting mode during hill climb: 35 kWh
- 3.Lowest cell voltage at EOL for exit coolant temperature below 95°C: 660 mV

Heat Exchangers	Dimensions and Details	Heat Loads	Radiator Fan 37 kW
HT Radiator	40″ (W) x 42″(H) x 2″ (D) Fins: louvered, 12-fpi, 10-mm height Tubes: 2-mm height	280 kW	Vehicle Speed: 30 mph
LT Radiator	40″ (W) x 35″ (H) x 2.5″ (D) Fins: louvered, 8-fpi, 20-mm height Tubes: 10-mm height	49 kW	Ambient T: 25⁰C
AC Condenser	40″ (W) x 28″ (H) x 0.75″ (D) Fins: plain, 12-fpi, 10-mm height Tubes: 2-mm height	12 kW	Air Flow Rate: 9.3 kg/s





## Parameter sensitivity analysis from cell model

- Summary of most crucial model parameters
  - ♦ Need to be measured with better accuracy and certainty
  - Suide for experimentalists

Туре	Operating conditions	Most crucial model parameters
Dry	80°C, 40% RH, air	$ORR\alpha_C$ , lonomer water uptake, ECSA, membrane conductivity
Normal	80°C, 80% RH, air	ORR $\alpha_c$ , lonomer water uptake, GDL porosity, ECSA
Oxygen starved	80°C, 80% RH, 5% O <sub>2</sub>	ORR $\alpha_c$ , lonomer water uptake, ECSA, oxygen reaction order
Flooded	80°C, 100% RH, air	CL saturation curve, ionomer contact angle, ORR $\alpha_c$ , GDL porosity & tortuosity



## **Analyzing Transport Properties Using Microelectrodes**

 Developed method for determining gas solubility and diffusivity in ionomer membranes

### Soluti-regime analysis used to extract parameters

- More accurate than previous methods of calculation
- Long-time: Numerical model for complicated geometry, extracts permeability of membrane
- Short-time: Cottrell equation modified to account for higher initial surface area, uses permeability to extract D
- Cottrell Equation<sup>1</sup>:
- $P=DK_g$  can then be used to determine the solubility,  $K_g$

 $I = \frac{nF\pi^{0.5} P C_g R^2 R_F}{D^{0.5} t^{0.5}}$ 

 Data demonstrate different trends for hydrogen and oxygen in terms of diffusivities





### Catalyst Durability Case Study





SEI(frame1)







- Shell thickness is pretty significant (> lnm ) for the 4-7nm particles
- Particles 10-50nm tend to be more Co rich than smaller particles, but with even thicker shells
- Some of the larger particles have a spongy structure (catastrophic Co loss) and are very Pt-rich
- USAXS and WAXS provide global analysis
- Significant particle size growth with more growth at the outlet
- Significant Co leaching observed



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## ASTWG

#### Pt:- PSD

### **PtCo PSD**



- Significant particle size growth with more growth at the outlet
- Significant Co leaching observed



		WAXS Peak	
	USAX	(220)	
	particle size	Stdev	Particle size
Sample	(nm)	(nm)	(nm)
Inlet A	6.53	1.35	10.01
Inlet B	7.53	1.19	10.92
Middle	7.34	1.36	10.40
Outlet	6.42	3.33	<sup>a</sup> 12.21
Outlet			ª70.11
Outlet			<sup>b</sup> 16.57

	USAXS		WAXS Peak (220)	
ample	particle size (nm)	Stdev (nm)	Particle size (nm)	% composition Pt/Co
<b>/</b> iddle	6.53	1.36	4.85	92.1/7.9
Aiddle			14.59	100/0
Dutlet_A	10.53	3.46	4.47	94.5/5.5
Dutlet_ A			15.35	100/0
Dutlet_ B	9.86	3.4	4.50	93.6/6.4
Dutlet_B			14.21	100/0



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### Automated data acquisition and analysis in STEM



- Automated image acquisition software purchased for FEI Talos TEM
  - Instrument runs autonomously overnight acquiring dozens of images and EDS maps
  - Sustom python codes under development for handling these large data sets for automated particle size and ionomer distribution measurements



### Approach: Suppressing Pt Dissolution to Enhance Durability ANL / UC Irvine: Vojislav Stamenkovic

Establishing the baseline for Pt dissolution



### intrinsic Pt dissolution normalized to Hupd

### Eliminated Pt dissolution up to 1.2V vs. RHE



### Foundation of the mechanism to eliminate Pt dissolution



#### subsurface Au facilitates Pt surface texturing towards (111) PtAu nanoparticles



PtAu in MEA: ECSA and MA loss: ~20% after 30K cycles

## **Pt Loading**

- Kinetic improvements with increased loading from 0.06 to 0.25
- In high H2 consumption region there is currently minimal improvement with increased Pt loading
- More baseline data coming with 50 wt% PtCo/HSC (Umicore) and 50 wt% Pt/HSC (TKK)
  - Need both materials and integration solutions
  - Need to keep metal (Pt) wt% high
    - Keep carbon loading below ~0.3 mg/cm<sup>2</sup>

### 30 wt%PtCo/HSC Umicore



### **Dictating Thin films/ Membrane Properties**

Nafion films/membranes prepared from high water concentration dispersions have more interconnected and ordered networks


## Ionomer EW trends validated via ex-situ experiments

Results confirm the impact of EW on ionomer thin-film permeability and catalyst poisoning Confirm direct correlation between *ex-situ* model experiments and *in-situ* performance trends

- Catalyst poisoning trends
- CO displacement: Higher anion adsorption with low EW ionomers
- GISAXS: Low EW ionomer have higher intensity at low  $\chi$  higher anisotropy

Thin-film Permeability trends

In-situ (conductivity) and ex-situ (ellipsometry) measurements confirm higher water uptake with low EW





## **Neutron Microscopy of Water Transport Phenomena**



**Operando images of the Mirai** 



NIST neutron imaging team: Eli Baltic (left), David Jacobson, Daniel Hussey (PI), and Jacob LaManna (right)

- Neutrons readily penetrate several cm of common metals, but have high sensitivity to water
- NIST's neutron and X-ray tomography (NeXT) system will be upgraded fall 2021 (lower right)
  - Higher energy and finer spot sized X-ray source extend application range
  - Neutron detector with improved time and spatial resolution
  - Solution by Dose reduction algorithms enable 1 hour acquisition times for 3D water content
- A neutron microscope is anticipated for the end of FY2022
- With spatial resolution ~3 μm, and time resolution 1s, this will nearly raise neutron imaging to the level of synchrotrons



"Plug and Play" support for full scale test sections for testing M2FCT materials



## M2FCT Component Integration - Manufacturing

- Understand impact of ink formulation and processing on (a) coating quality (b) electrode structure (c) performance Explore novel electrode structures to improve durability and durability
- Develop correlations between catalyst/ink parameters and ink macro behaviors (e.g., rheology)
- Understand impact of MEA/component defects on durability (and durability studies)

- Ink additives to modify porosity, structural integrity, and cracking
- Multilayer structures

Develop and demonstrate methods for in-process ink QA





Viscosity [Pa-s]



## **Flow Fields & Orientation**





flow orientation didn't affect the performance
minimal impact of flow field

>20-40 mV improvement from flow orientation >~20-40 mV from flow field

> Need to establish common platform for materials down selection assessment