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# Advanced AEMs with Tunable Water Transport for PGM-Free AEMFCs

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**Project ID #  
FC308**

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# Overview

## Timeline and Budget

- ❖ Project Start Date: 10/01/18  
Agreement authorized 12/17/2018
- ❖ Project End Date: 09/30/20
- ❖ Total Project Budget: \$1,278,452
  - Total Federal Share: \$1,000,000
  - Total Recipient Share: \$278,452
  - Total DOE Funds Spent\*: \$165,068

\* As of 3/01/19

## Barriers

- A. Durability – focused on demonstrating moderate durability of AEMFCs based on understanding of water transport
- B. Cost – enabling AEMFCs will lower the cost of the catalysts and the membranes
- C. Performance – understanding water transport is key to high performance AEMFCs

## Funded Partners

- ❖ Penn State University
- ❖ University of South Carolina
- ❖ National Renewable Energy Laboratory
- ❖ 3M Corporation

# Relevance

## **Objectives: Over the course of this 24-month program, our team will:**

- ❖ Develop novel poly(olefin) AEM chemistries with tunable water transport. In order to facilitate high AEMFC performance, they will have the following properties:
  - OH<sup>-</sup> conductivities greater than 60 mS/cm at 60 °C, 100 % RH
  - Less than 10% degradation in conductivity after 5000 hours in 1 M NaOH at 60 °C and 2000 hours in 1 M NaOH at 80 °C
  - Water diffusion coefficient >  $5 \cdot 10^{-6}$  cm<sup>2</sup>/s (50% improvement over existing AEMs)
  
- ❖ Incorporate these novel ionomers into mechanical supports and integrate the resulting membranes into AEMFCs. During operation inside the AEMFC, the membranes will have:
  - ASR values less than 100 mOhm·cm<sup>2</sup> over 2000 hour operation
  - Water flux greater than  $2 \cdot 10^{-5}$  mol H<sub>2</sub>O/cm<sup>2</sup>·s – in order to be able to back-diffuse 80% of produced + electro-osmotic water from anode to cathode @ 600 mA/cm<sup>2</sup>
  
- ❖ Demonstration of all of the following DOE metrics in a single MEA with H<sub>2</sub>/O<sub>2</sub> fuel:
  - Greater than 2000 hours of AEMFC operation at 600 mA/cm<sup>2</sup>
  - Operating voltage greater than 0.6 V with less than 10% decay over 2000 hours
  - Operating T ≥ 60 °C and P ≤ 1.5atm<sub>a</sub> with PGM loading less than 0.125 mg<sub>PGM</sub>/cm<sup>2</sup>

# Approach

## Focus on improved water management in AEMFCs

- ❖ Synthesize new polyolefin-based membranes with high water diffusion coefficients (2x of current AEMs,  $>5 \times 10^{-6} \text{ cm}^2/\text{s}$  by PFG-NMR) and thicknesses of  $\sim 20$  microns using support structures.
- ❖ Optimize electrode formulation to pair with new membranes using current state-of-the-art knowledge on AEMFC electrodes.
- ❖ Control cell conditions and measure water balance to develop a full understanding of how water transport influences cell performance and durability.
- ❖ Use neutron radiography and cell water balance measurements to develop water transport-durability correlations.

# Major Milestones and Go/No-Go

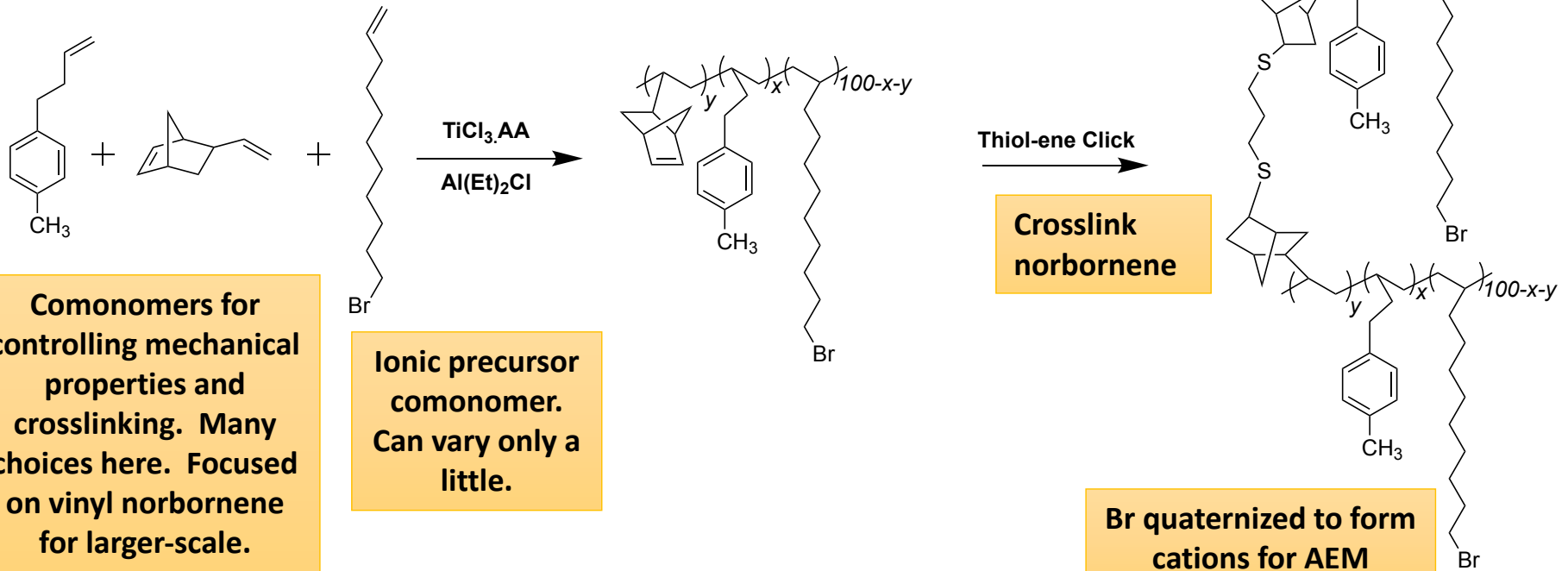
## Month/Quarter

<b>M6/Q2</b>	Performance Milestone	AEMFC steady-state operation at 600 mA/cm <sup>2</sup> . Cell Voltage > 0.6 V. H <sub>2</sub> /O <sub>2</sub> reacting gases; Cell T ≥ 60°C; Pressure ≤ 1.5 atm <sub>a</sub>
<b>M12/Q4</b>	Go/No-Go	500h AEMFC operation at 600 mA/cm <sup>2</sup> . Cell Voltage > 0.6 V. Anode/Cathode feed gas: H <sub>2</sub> /O <sub>2</sub> ; Cell T ≥ 60°C; Anode/Cathode pressure ≤ 1.5 atm <sub>a</sub>
<b>M18/Q6</b>	Performance Milestone	500 h AEMFC operation at 600 mA/cm <sup>2</sup> . Cell Voltage > 0.6V. Anode/Cathode feed gas: H <sub>2</sub> /O <sub>2</sub> ; Cell T ≥ 60°C; Anode/Cathode pressure ≤ 1.5 atm <sub>a</sub> . Total MEA PGM loading ≤ 0.125 mg/cm <sup>2</sup> . 5 cm <sup>2</sup> active area
<b>M21/Q7</b>	Progress Measure	500h AEMFC operation at 600 mA/cm <sup>2</sup> . Cell Voltage >6V. H <sub>2</sub> /Air(CO <sub>2</sub> -free); Cell T ≥ 60°C; Anode/Cathode Pressure ≤ 1.5 atm <sub>a</sub>
<b>M24/Q8</b>	Performance Milestone	AEMFC steady-state operation at 600 mA/cm <sup>2</sup> with cell voltage > 0.6 V. H <sub>2</sub> /Air (400 ppm CO <sub>2</sub> ) feed gases; Cell T ≥ 60°C; Anode/Cathode pressure ≤ 1.5 atm <sub>a</sub>
<b>M24/Q8</b>	End-of-Project Goal	2000 h AEMFC continuous operation at 600 mA/cm <sup>2</sup> . Cell Voltage > 0.6 V, less than 10% voltage fade. Anode/Cathode feed gases: H <sub>2</sub> /O <sub>2</sub> ; Cell T ≥ 60°C; Anode/Cathode pressure ≤ 1.5 atm <sub>a</sub> ; Total MEA PGM loading ≤ 0.125 mg/cm <sup>2</sup> ; 50 cm <sup>2</sup> active area.

Current status: Can achieve M6 performance metrics with first-generation membranes. Currently working on measuring membrane water diffusion coefficients and optimizing supported membranes. Will begin lifetime testing in M7.

# Accomplishments and Progress: Polymer Synthesis

## Synthetic route for polyolefin-based crosslinked AEMs



M3/Q1	Membrane Milestone	≥ 2 AEM compositions with conductivity greater than 40 mS/cm at 60 °C in liquid water and water diffusion coefficient greater than $2 \cdot 10^{-6}$ cm <sup>2</sup> /s fabricated and delivered for cell testing
M3/Q1	Progress Measure	≥ 2 ionomer dispersions/powder samples sent to USC/NREL for cell testing

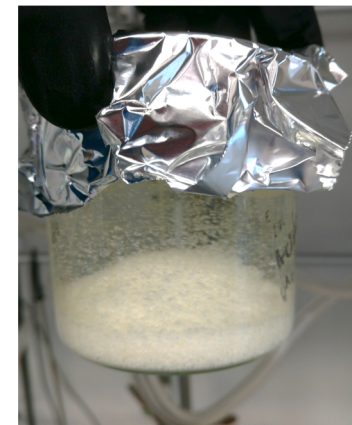
# Accomplishments and Progress: Polymerization Batches

Control AEM – 3 batches	M.W.	eq	mass (g)
11-bromo-1-undecene	233.19	1	1.063
4-phenyl-1-butene	132.20	2	3.52
TiCl <sub>3</sub> ·AA 75%	198.72		0.05
		1 mL/mg	
AlEt <sub>2</sub> Cl pure	120.56	TiCl <sub>3</sub>	
Toluene (anhydrous)			50 mL

Novel AEM – Low IEC – 2 batches	M.W.	eq	mass (g)
11-bromo-1-undecene	233.19	1	2
5-vinyl-1-norbornene	120.19	5	5.2
TiCl <sub>3</sub> ·AA	198.72		0.05
		1 mL/mg	
AlEt <sub>2</sub> Cl 1.0 M in hexanes	120.56	TiCl <sub>3</sub>	
Toluene (anhydrous)			50 mL

Novel AEM – High IEC – 3 batches	M.W.	eq	mass (g)
11-bromo-1-undecene	233.19	1	2
5-vinyl-1-norbornene	120.19	5	5.2
TiCl <sub>3</sub> ·AA	198.72		0.05
		1 mL/mg	
AlEt <sub>2</sub> Cl 1.0 M in hexanes	120.56	TiCl <sub>3</sub>	
Toluene (anhydrous)			50 mL

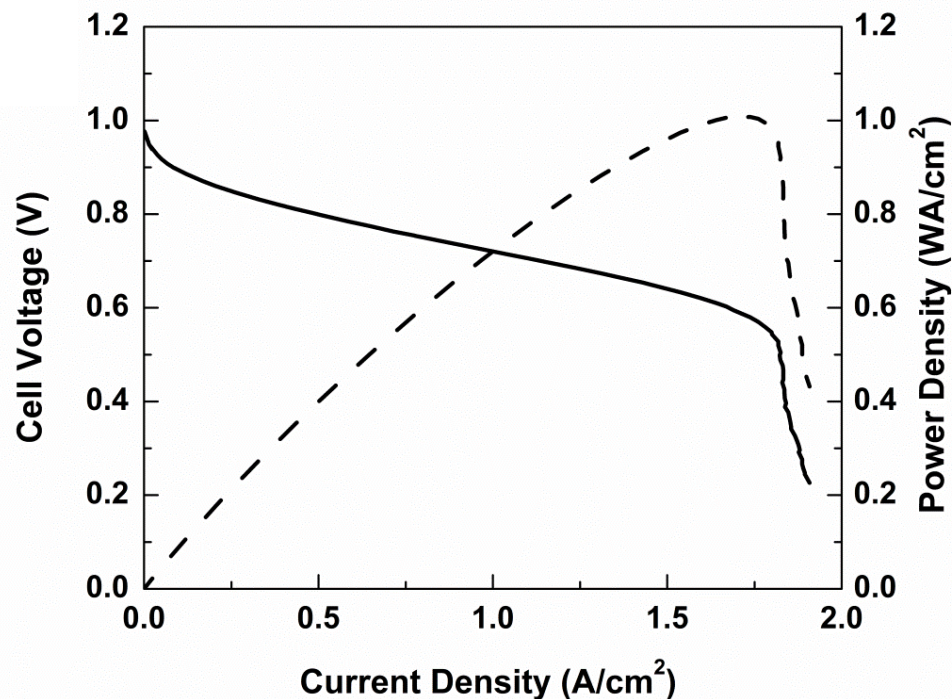
- ❖ Over 80 polymerization batches conducted.
- ❖ 8 successful, on target batches shown at left.
- ❖ Yields approaching 60 %
- ❖ IECs between 1.5 and 12.5 meq/g targeted.
- ❖ Membrane IEC, conductivity, water transport, and stability currently being measured.
- ❖ 4 g batch of polymer shown below. Increasing scale currently.



Current status: Working on supported membranes with larger polymer batches. More samples being sent to project partners.



# Accomplishments and Progress: Cell Testing Demonstrations



- ❖ Powdered ionomer in electrodes
- ❖ Cathode: 0.50 mg<sub>Pt</sub>/cm<sup>2</sup> Alfa Aesar HiSPEC 4000, Pt nominally 40%wt., supported on Vulcan XC-72R carbon
- ❖ Anode: 0.70 mg<sub>Pt-Ru</sub>/cm<sup>2</sup> Pt-Ru catalyst (Alfa Aesar HiSPEC 10000, Pt nominally 40%wt., and Ru, nominally 20%wt., supported on Vulcan XC-72R carbon
- ❖ 60 °C cell temperature, H<sub>2</sub>/O<sub>2</sub> reacting gases at 1.0 L/min.

Current status: Membrane testing for durability in progress to meet next milestone. Electrode work in progress to meet project goals.



# Responses to Previous Year Reviewers' Comments

- ❖ New project commenced in late 2018.
- ❖ Project not reviewed last year.

# Collaboration & Coordination

- ❖ Project collaborators:
  - Prime – Penn State University
  - Sub Recipients –
    - ❑ University of South Carolina
    - ❑ National Renewable Energy Laboratory
    - ❑ 3M Corporation
- ❖ University of South Carolina is responsible for electrode formulation, cell testing, and water transport studies – including neutron radiography
- ❖ National Renewable Energy Laboratory is responsible for lifetime testing and water balance studies
- ❖ 3M Corporation is responsible for membrane coating and supported membranes
- ❖ Coordination is performed through regular meetings and teleconferences. All project partners have worked together previously and have joint publications.



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# Remaining Challenges and Barriers

- ❖ Need larger-scale polymer synthesis for coating and supported membranes. Working with vinyl norbornene and single cations to keep synthesis simple.
- ❖ Larger-scale samples will enable more lifetime testing and neutron radiography studies of water transport.
- ❖ Lifetime still needs to be proven out at lower loadings to meet Year 1 Go/No-Go.
- ❖ Electrode formulation, membrane thickness, and water transport studies will enable a wholistic understanding of how water transport in the cell influences performance and durability.

# Proposed Future Work

## ❖ Rest of this year - FY19

- Synthesize larger-scale batches of polymer with vinyl norbornene motif and fabricate supported membranes.
- Continue to optimized electrode structures and cell conditions to meet milestones and Year 1 Go/No-Go on performance and durability at required loadings.
- Measure water transport in membranes using PFG-NMR and connect to cell water transport observations using water balance measurements.

## ❖ Next year - FY20

- Fabrication of high-performance supported membranes and optimization of electrode structures and cell conditions will allow for progress on Year 2 milestones.
  - Develop strategies for increasing durability through modifying cell water transport.
  - Develop wholistic picture of water transport in AEMFCs using neutron radiography.
- 
- Risk will be mitigated by taking advantage of state-of-the-art catalyst for alkaline membranes that are reported.
  - Major risks will be to approach required catalyst loadings while still reaching durability targets.

*Any proposed future work is subject to change based on funding levels.*

# Technology Transfer Activities

- ❖ 3M and Penn State have filed joint IP under past programs. Considering joint IP on new material composition for this work.

# Summary Slide

- ❖ Key early data indicates success in achieving performance metrics. Still catalyst layer work and cell conditions to optimize for meeting loading and durability targets.
- ❖ We have demonstrated 100s of hours of lifetime at 600 mA/cm<sup>2</sup> with previous polyolefin membranes in a collaboration between Penn State and U. South Carolina. Working to solidify the lifetime testing on current membranes with lower catalyst loadings.
- ❖ Larger scale synthesis is underway and will enable more membrane coating studies and lifetime testing.
- ❖ Work underway to meet Year 1 Go/No-Go.

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Anode/Cathode feed gas: H<sub>2</sub>/O<sub>2</sub>; Cell T ≥ 60°C; Anode/Cathode pressure ≤ 1.5 atm<sub>a</sub>