

Proton-Conducting Ceramic Electrolyzers for High-Temperature Water Splitting



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April 30, 2019

2019 DOE Hydrogen and Fuel Cells
Program Review

Project ID# p177

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Timeline

- Project Start Date: 10/01/2018
- Project End Date: 09/30/2020

Budget

- Total Project Budget: \$1,875,000
- Total Recipient Share: \$ 375,000
- Total Federal Share: \$1,500,000
- Total DOE Funds Spent*: \$ 75,000

* Estimated as of 3/1/19

Barrier

- Key barriers addressed in the project are:
 - F. Capital Cost
 - G. System Efficiency and Electricity Cost
 - J. Renewable Electricity Generation Integration

Partner

- FuelCell Energy (FCE) – Project Lead
- Colorado School of Mines (CSM)
- Versa Power Systems (VPS)

Objective:

Development of efficient and durable high-temperature water splitting (HTWS) systems for production of hydrogen at a cost less than \$2/kg H₂, using proton conducting ceramic electrolytic cell (PCEC) technology at a temperature $\geq 500^{\circ}\text{C}$. Technical performance targets for the electrolysis stack include:

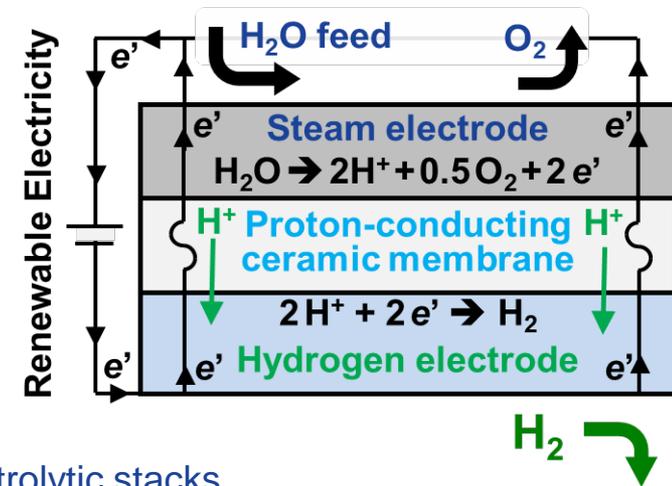
- Specific resistance of $\leq 0.30 \text{ } \Omega\text{-cm}^2$
- Stack electrical efficiency $> 95\%$ LHV H₂ at current density $> 1 \text{ A/cm}^2$
- Stack lifetime of ≥ 7 years

Project Goals:

- Increase PCEC performance by achieving Faradaic efficiency $> 95\%$, electrical efficiency $> 95\%$, and area-specific resistance $< 0.15 \text{ } \Omega\text{-cm}^2$ at 1 A/cm^2 and 550°C
- Reduce PCEC degradation $< 1\%$ / 1000 hours
- Scale-up cell area (up to $10 \times 10 \text{ cm}^2$) and develop manufacturing process
- Demonstrate operation of a PCEC stack for $\geq 1 \text{ kg/day}$ H₂ production, $> 95\%$ electric efficiency (LHV) at $\geq 1 \text{ A/cm}^2$ with degradation $< 3\%/1 \text{ khr}$
- Perform Techno-Economic analysis and determine cost of hydrogen production with a target of \$2/kg

The project seeks new protonic-ceramics to drive down operating temperature

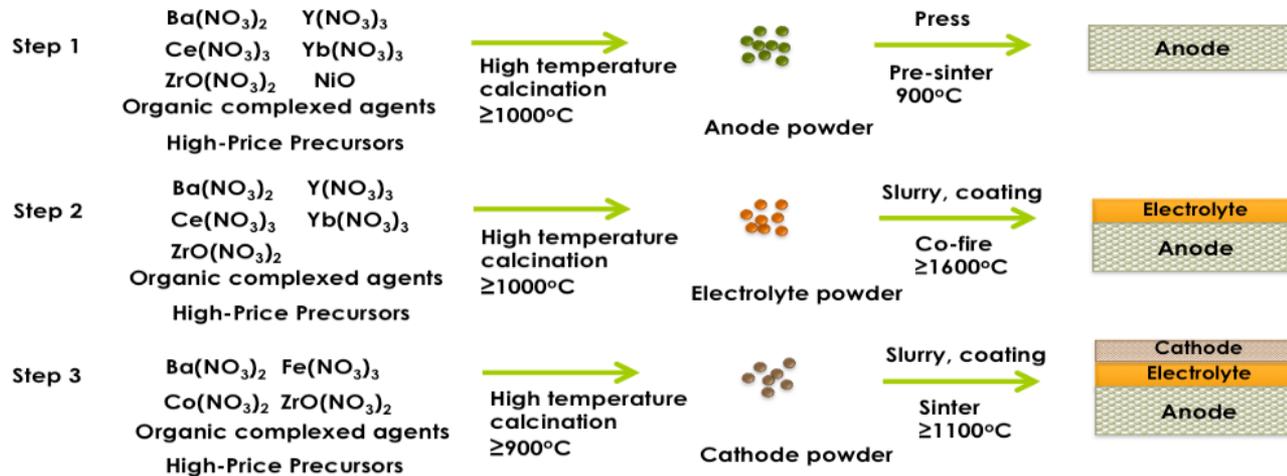
- Conduct optimization of the air electrode under electrolysis operation, both from performance and degradation standpoints.
- Perform optimization of the electrolyte composition and morphology to establish long-term stability and mitigate current leakage.
- Develop database of physical and mechanical properties to be used in P-SOEC technology scale-up and stack design.
- Develop manufacturing processes for P-SOEC cells using high-yield ceramic processing technologies, including tape casting and screen printing.
- Scale cell active area up to 100 cm² suitable for commercial electrolytic stacks.
- Develop P-SOEC stack design and specifications for stack components including seals, interconnects, compression plates, manifolds, and contact media.
- Develop stack manufacturing process including factory conditioning and acceptance tests.
- Develop a flow sheet and process flow diagram for a P-SOEC system.
- Design and build a P-SOEC stack with capacity of at least 1 kg H₂/day for validation of project objectives' performance targets.
- Complete the Factory Cost estimate of the P-SOEC system for DOE's H2A analysis.
- Complete DOE H2A analysis for P-SOEC system to verify achievement of program cost target of less than \$2/kg H₂ for hydrogen production.



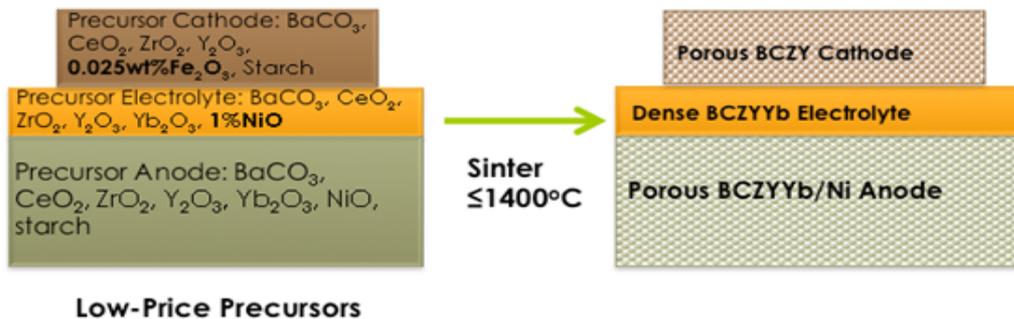
Milestone #	Project Milestones	Type	Task Completion Date (Project Quarter)				Progress Notes
			Original Planned	Revised Planned	Actual	Percent Complete	
1.1.1	Down-select PCEC electrolyte	Milestone	6/30/19			75%	
1.1.2	Demonstrate Faradaic efficiency > 85%, Electric efficiency > 75% at 1 A / cm ²	Milestone	9/30/19		12/31/18	100%	Complete
1.1.3	Demonstrate Faradaic efficiency > 90%, electrical efficiency > 80%, and area-specific resistance < 0.3 Ω-cm ² at 1 A / cm ² at 550 °C	Milestone	12/31/19			50%	
1.1.4	Demonstrate Faradaic efficiency > 95%, electrical efficiency > 85%, and area-specific resistance < 0.15 Ω-cm ² at 1 A / cm ² at 550 °C	Milestone	6/30/20			5%	
1.2.1	Initiate 1000-hour PCEC fuel- and steam-electrode baseline degradation tests	Milestone	12/31/18		12/31/18	100%	Complete
1.2.2	Initiate 1000-hour PCEC MEA baseline-degradation tests	Milestone	3/31/19			10%	
	Demonstrate P-SOEC MEA with degradation rate of <5%/1000 hr and Faradaic efficiency of >95% at 1 A/cm ² at ≤550°C	Go-No-Go	9/30/19				Not started
1.2.3	Demonstrate PCEC electrode degradation rates < 2% / 1000 hours	Milestone	12/31/19			0%	Not started
1.2.4	Demonstrate PCEC MEA degradation rates < 2% / 1000 hours	Milestone	3/31/20			0%	Not started
1.2.5	Demonstrate PCEC electrode degradation rates < 1% / 1000 hours	Milestone	6/30/20			0%	Not started
1.2.6	Demonstrate PCEC MEA degradation rates < 1% / 1000 hours	Milestone	9/30/20			0%	Not started
1.3.1	Establish baseline performance of industrially manufactured protonic ceramic electrolytic cell with ≥ 16 cm ² active area	Milestone	9/30/19			0%	Not started
1.4.1	Performance validation of large-area cell (at least 5x5 cm and up to 10x10 cm) equal to or better than the baseline and demonstrate Faradaic efficiency >95% at current density of 1 A/cm ² at 550 °C	Milestone	12/31/19			0%	Not started
2.1.1	Stack modeling complete and determining the effects of operating conditions	Milestone	9/30/19			0%	Not started
.2.1	Manufacture a tall stack for ≥ 1 kg H ₂ / day	Milestone	6/30/20			0%	Not started
2.3.1	Achieve PCEC stack performance >95% eff (LHV) at ≥1A/cm ² and degradation <3%/1khr	Milestone	9/30/20			0%	Not started
3.1.1	Develop a process flow diagram based on the selected PCEC system design.	Milestone	12/31/19			0%	Not started
3.3.1	Complete H ₂ A analysis and determine the cost of hydrogen production with a target of \$2/kg H ₂	Milestone	9/30/20			0%	Not started

Simple, cost-effective cell fabrication using Solid-State Reactive Sintering (SSRS) developed for Proton Conducting Fuel Cells (PCFC) will be applied in this project to fabricate electrolytic cells (PCEC)

(a) Traditional Approach

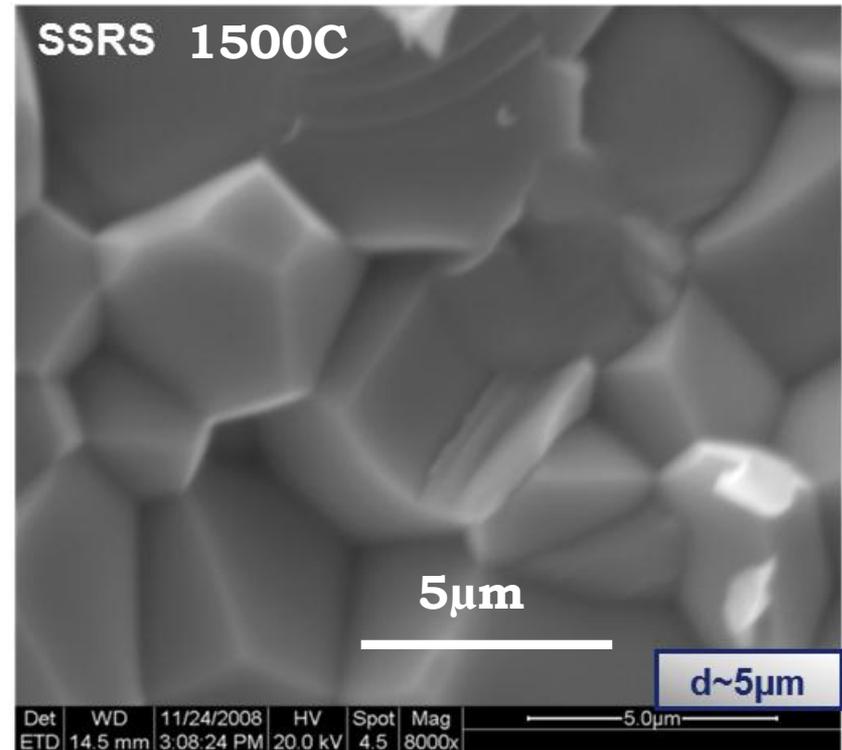
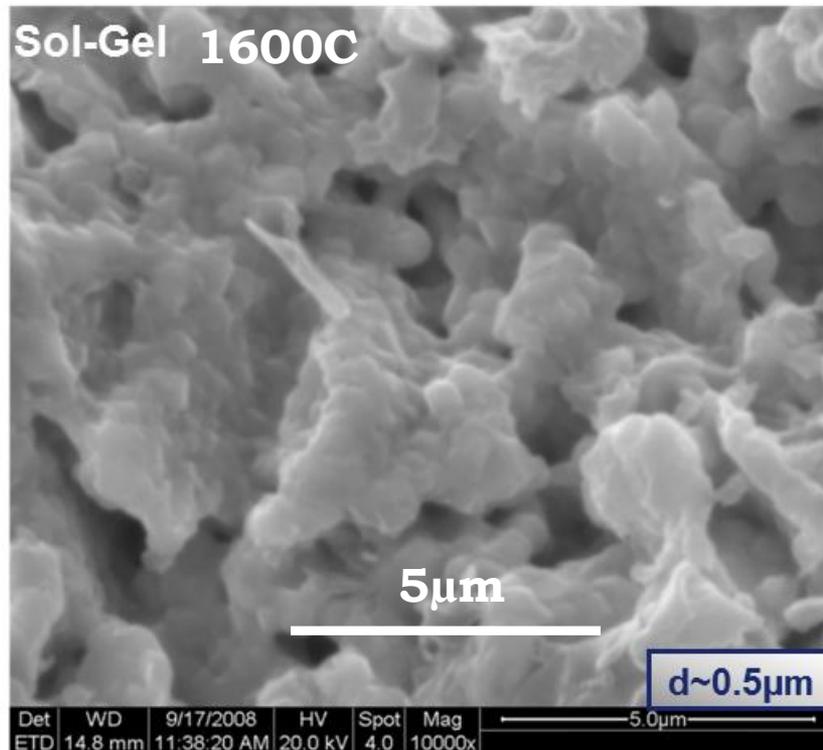


(b) SSRS Approach



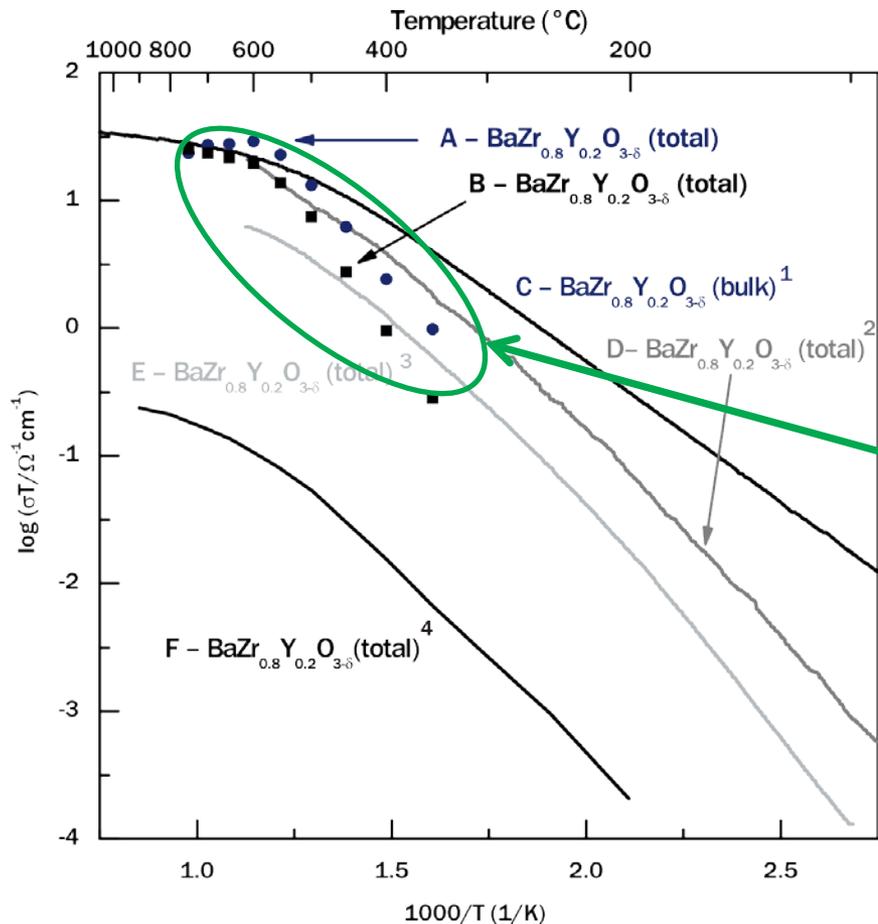
Colorado School of Mines (CSM)
 U.S Patent Application: US
 2016/0036064 A1 "Cost Effective
 Solid-State Reactive Sintering
 Method for Protonic Ceramic Fuel
 Cells"

SSRS produces denser, larger-grained BZY20 at significantly lower sintering temperatures than the more complex and expensive sol-gel process alternative



SSRS with 1wt% NiO sintering aid, both samples sintered for 24 hours

Arrhenius plots of total conductivity for BZY20 pellets obtained by SSRS method with 2wt% NiO as sintering aid by sintering at 1500°C for 24 hrs, and compared with total or bulk conductivities for recent reported BZY20 pellets



Conductivities at 600°C

A. Wet Ar – 33 mS/cm

B. Dry Ar – 22 mS/cm

SSRS materials meet or exceed best literature reports

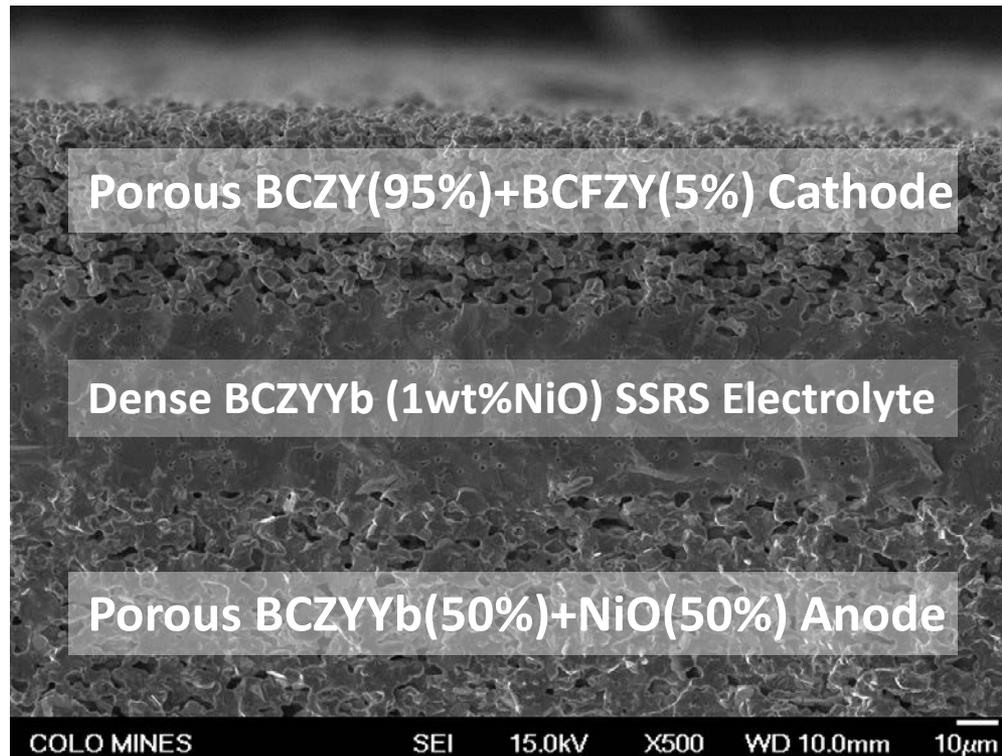
[1] K.D. Kreuer et al, Solid State Ionics, 2001, 145, 295

[2] Y. Yamazaki et al, Chem. Mater., Articles ASAP

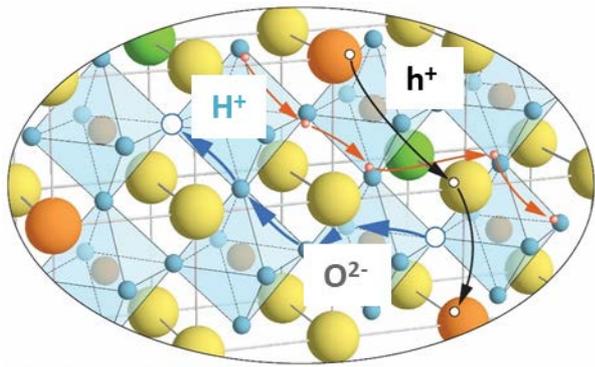
[3] P. Babilo et al, J. Mater. Res., 2007, 22(5), 1322

[4] S.W. Tao et al, Journal of Solid State Chemistry, 2007, 180, 3493

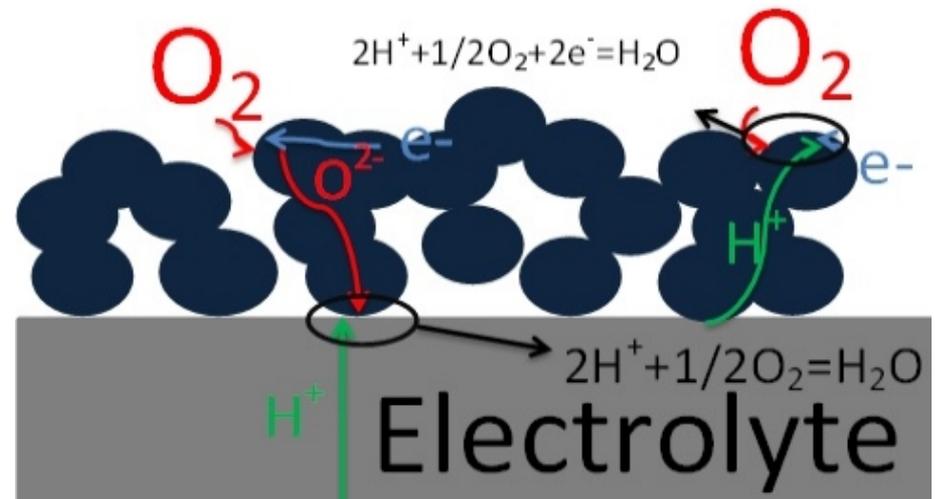
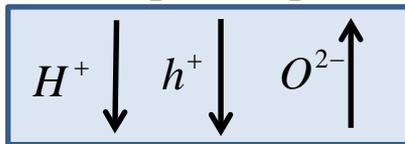
Produced from raw unreacted powder precursors of BaCO_3 , CeO_2 , ZrO_2 , Y_2O_3 , Yb_2O_3 , and NiO , CeO_2 , and Fe_2O_3 in a single-step via SSRS (1350°C for 12hrs)



CSM Team has developed a triple conducting oxide based on BCFZY material. Co/Fe doping has enabled hole conduction within BZY structure



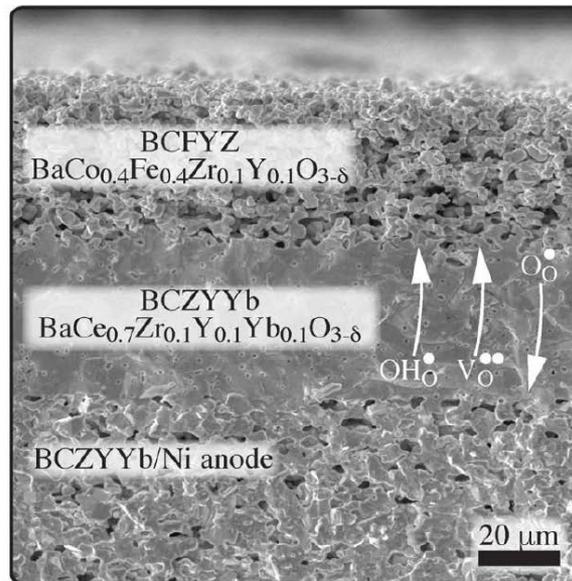
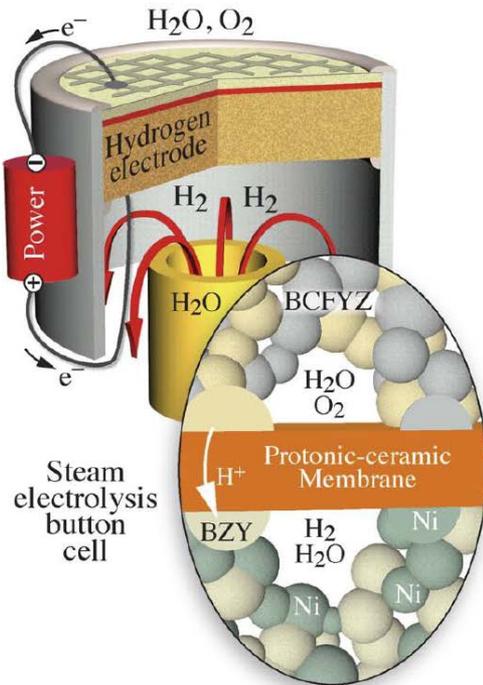
A-site cation: Ba
B-site TM dopants: Co, Fe
B-site acceptor dopant: Y



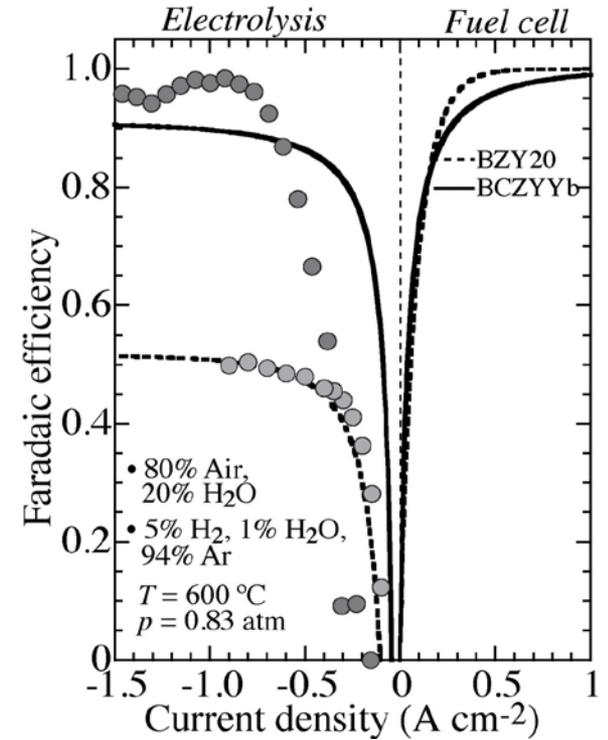
CSM U.S. Provisional Patent Application US 14/991027 “Triple Conducting Cathode Material for Intermediate Temperature Proton Conducting Electrochemical Devices”

Key Breakthrough: The Electrolyte Matters for Electrolysis Performance!

Test results have confirmed modeling work that at temperatures below 600°C, BCZYYb can achieve high faradaic efficiencies (i.e., low electronic leakage) as an electrolyzer membrane.

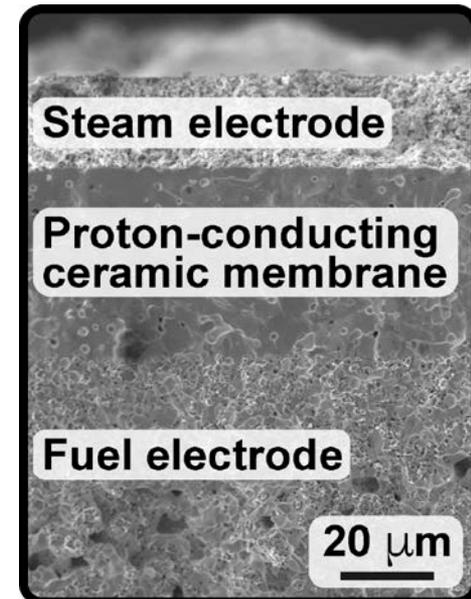


Protonic-ceramic membrane-electrode assembly



Milestone M1.1.1: Downselect electrolyte composition has progressed (75% complete)

- Electrolyte Layer
 - $\text{BaCe}_{0.7}\text{Zr}_{0.1}\text{Y}_{0.1}\text{Yb}_{0.1}\text{O}_{3-d}$ (BCZYYb-7111)
 - Minimal electronic leakage at target operation
 - Also exploring BCZYYb-4411 composition
- Composite fuel electrode:
 - Ni + BCZYYb-7111 "cermet"
 - Mechanical support
- Composite steam electrode:
 - $\text{BaCo}_{0.4}\text{Fe}_{0.4}\text{Zr}_{0.1}\text{Yb}_{0.1}\text{O}_{3-d}$
 - 80 wt-% BCFZY-44111
 - 20 wt-% BCZYYb-7111

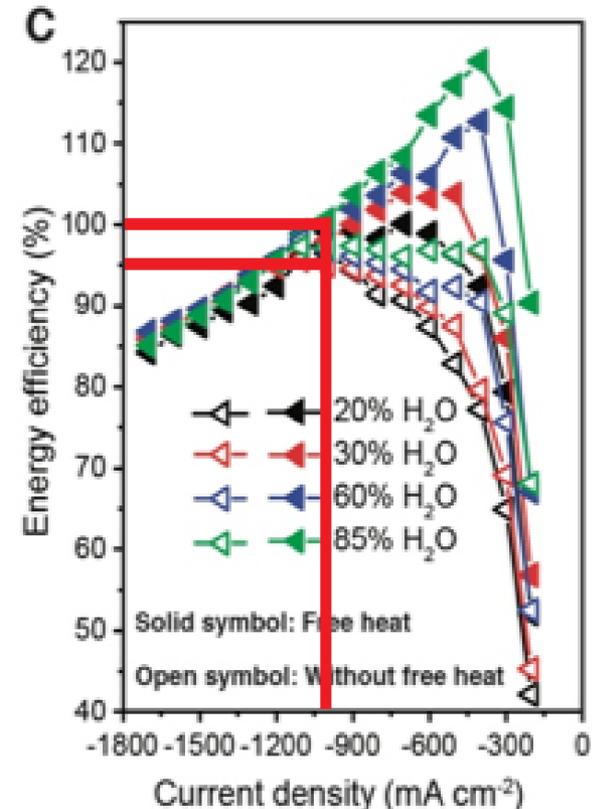
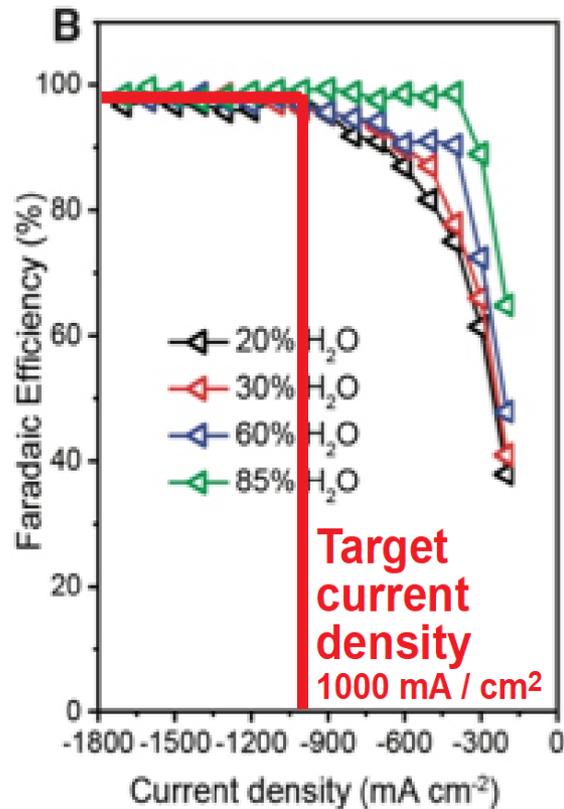
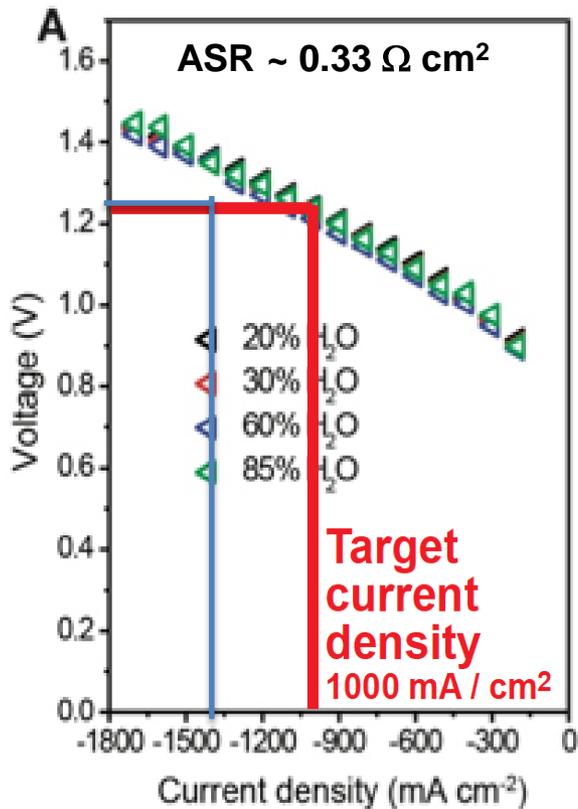


Milestone M1.1.2: Faradaic efficiency > 85% and electrical efficiency > 75% at 1 A / cm² were achieved

Polarization curve

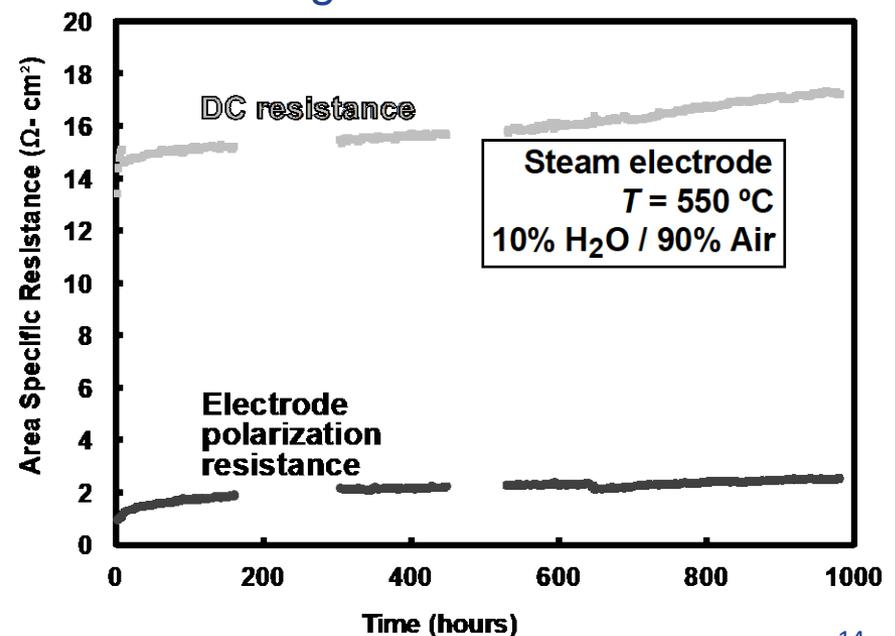
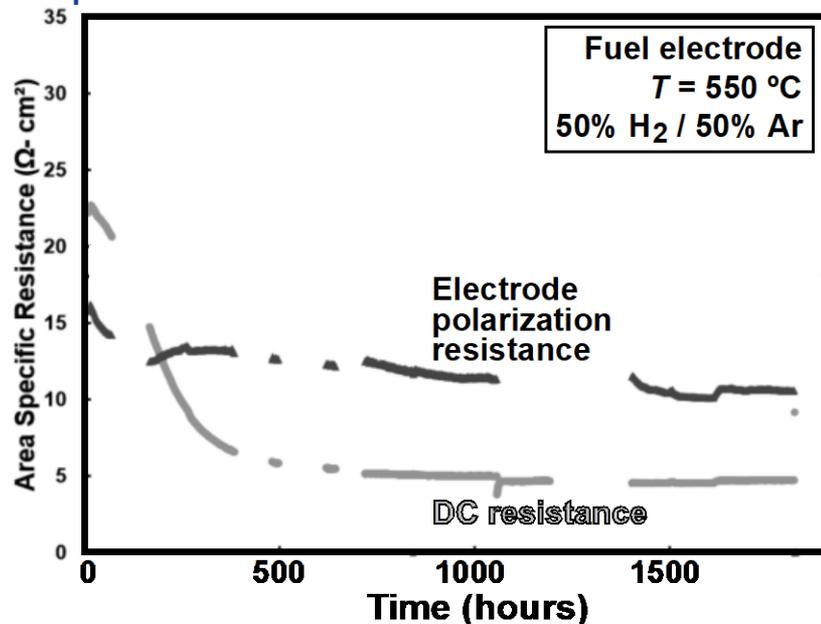
Faradaic efficiency

Energy efficiency



Milestone M1.2.1: 1000-hour PCEC fuel- and steam-electrode baseline degradation tests were completed

- Symmetric button cells were fabricated to measure the electrode performance degradations by AC impedance spectroscopy
- Negligible degradation was observed in the fuel electrode at the testing conditions of 550 °C and 50% H₂O / 50% Ar over a period of 1800 hours
- Steam electrode showed a measurable increase in both the DC and electrode-polarization resistance over the 1000 hours of testing



Degradation in fuel (left) and steam (right) electrodes over time

- This project was not reviewed last year

- **Colorado School of Mine (CSM)**

- R&D activities at CSM are led by Professors Neal Sullivan, Ryan P. O'Hayre, and Robert Braun. The CSM team is providing the following expertise:

- Fundamental solid Ionics and materials science
- Cell and multi-cell stack testing
- Performance optimization
- System and Techno-Economic Analysis (TEA)



- **Versa Power Systems (VPS), Operating as FuelCell Energy**

- VPS is providing the following expertise in the project:

- Cell materials & components
- Stack design
- Cell/stack pilot manufacturing and QC
- Cell/stack testing



Cell Pilot Manufacturing Processes at VPS: (Tape Casting, Screen Printing, and Co-sintering)

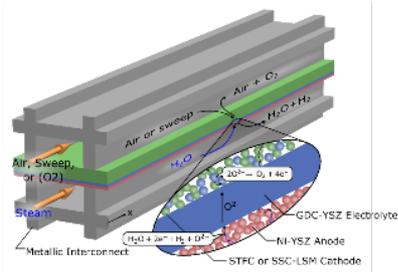
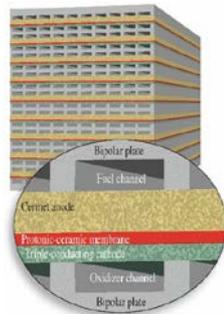
- Cell Performance
 - Develop understanding of cell performance degradation mechanisms
 - Develop degradation mitigation strategies and reduce cell performance degradation to <1%/1000 hours
 - Reduce specific cell resistance to < 0.15 ohm-cm²
 - Scale up of cell and manufacturing process to fabricate cells up to 10 x 10 cm in size and meeting the target electric efficiency of >95% (based on LHV)
- Stack Development
 - Develop stack models predicting the PCEC performance and temperature profiles
 - Fabricate a commercial prototype PCEC stack sized for 1 kg/day of H₂ production, meeting the performance targets of >95% efficiency (LHV) at ≥ 1 A/cm² and performance degradation of <3%/1000 hours
- Techno-economic Analysis
 - Develop cost-optimized system to meet \$2/kg H₂ target while meeting the overall system efficiency goal of 75% (LHV of H₂)

- Investigate cell performance degradation mechanisms and develop mitigation strategies to reduce cell performance loss with time to $< 1\%/1\text{hr}$
- Fabricate and build cells with active area up to $>100\text{ cm}^2$
- Complete stack design and initiate fabrication of stack hardware components for building a stack for 1 kg/day H_2 production
- Continue design of system process flow diagram and complete modeling of stack and sizing of the balance-of-equipment equipment:
 - Develop single-cell PCEC model
 - Update model and extend to stack design as cell materials/architecture become available
 - Validate cell model

Any proposed future work is subject to change based on funding levels

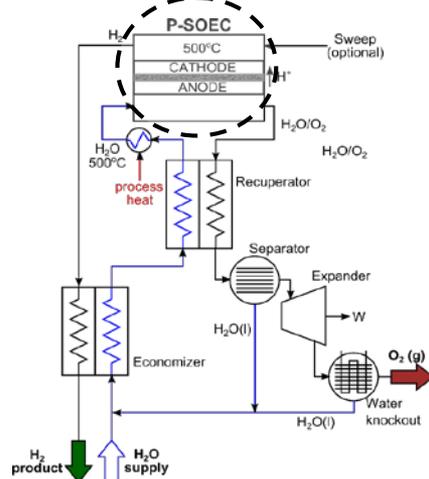
Planned multi-scale modeling will move from physical models to process systems to TEA and Life-Cycle-Analysis (LCA)

Stack Modeling

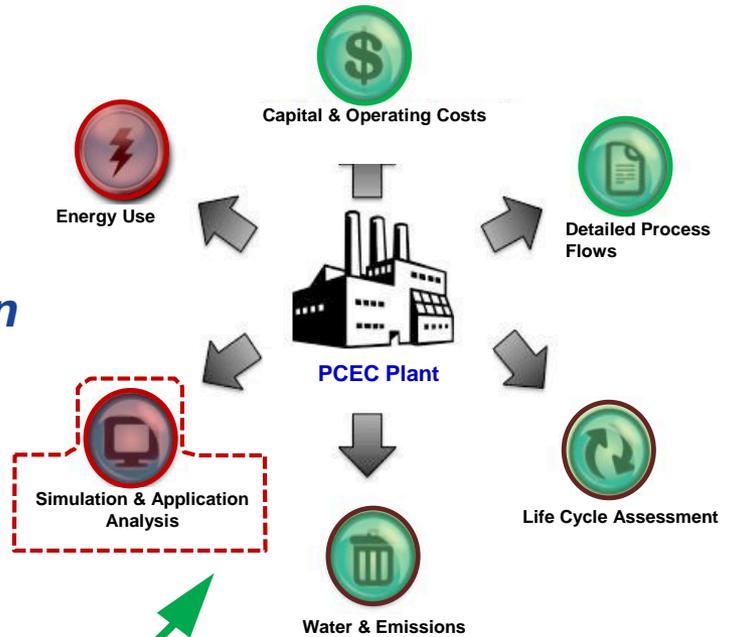


Cell Modeling

Process System Design

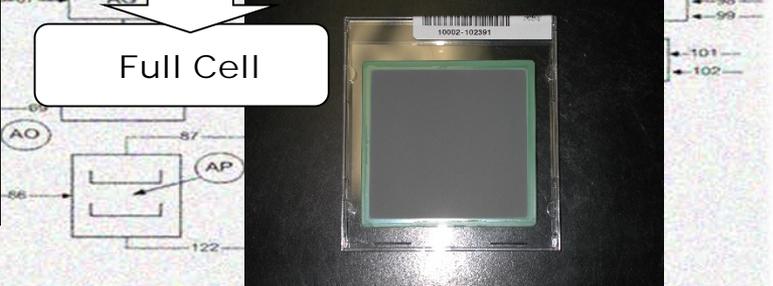
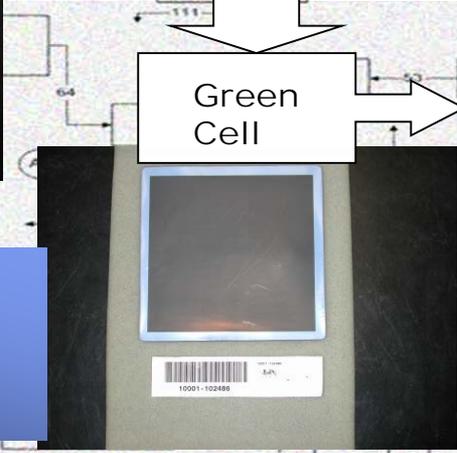
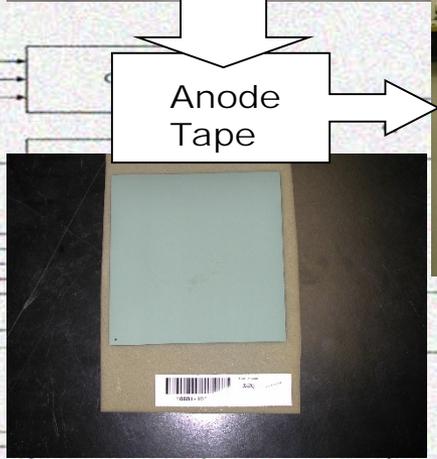
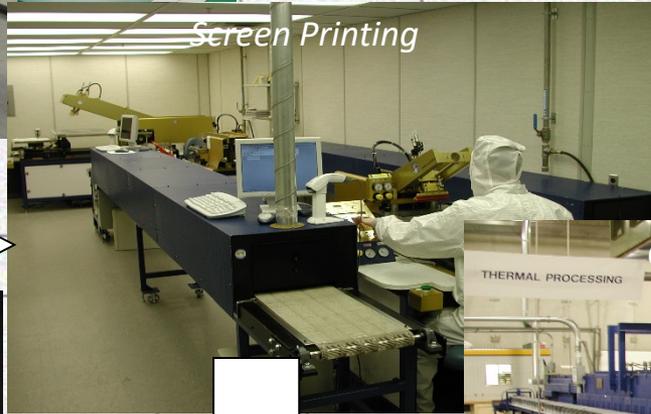
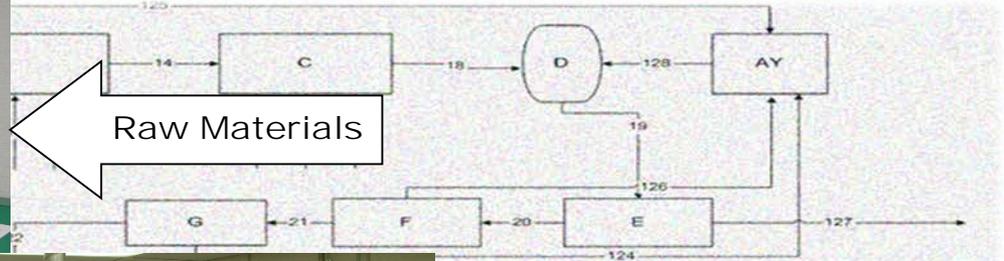


Systems-level TEA & LCA

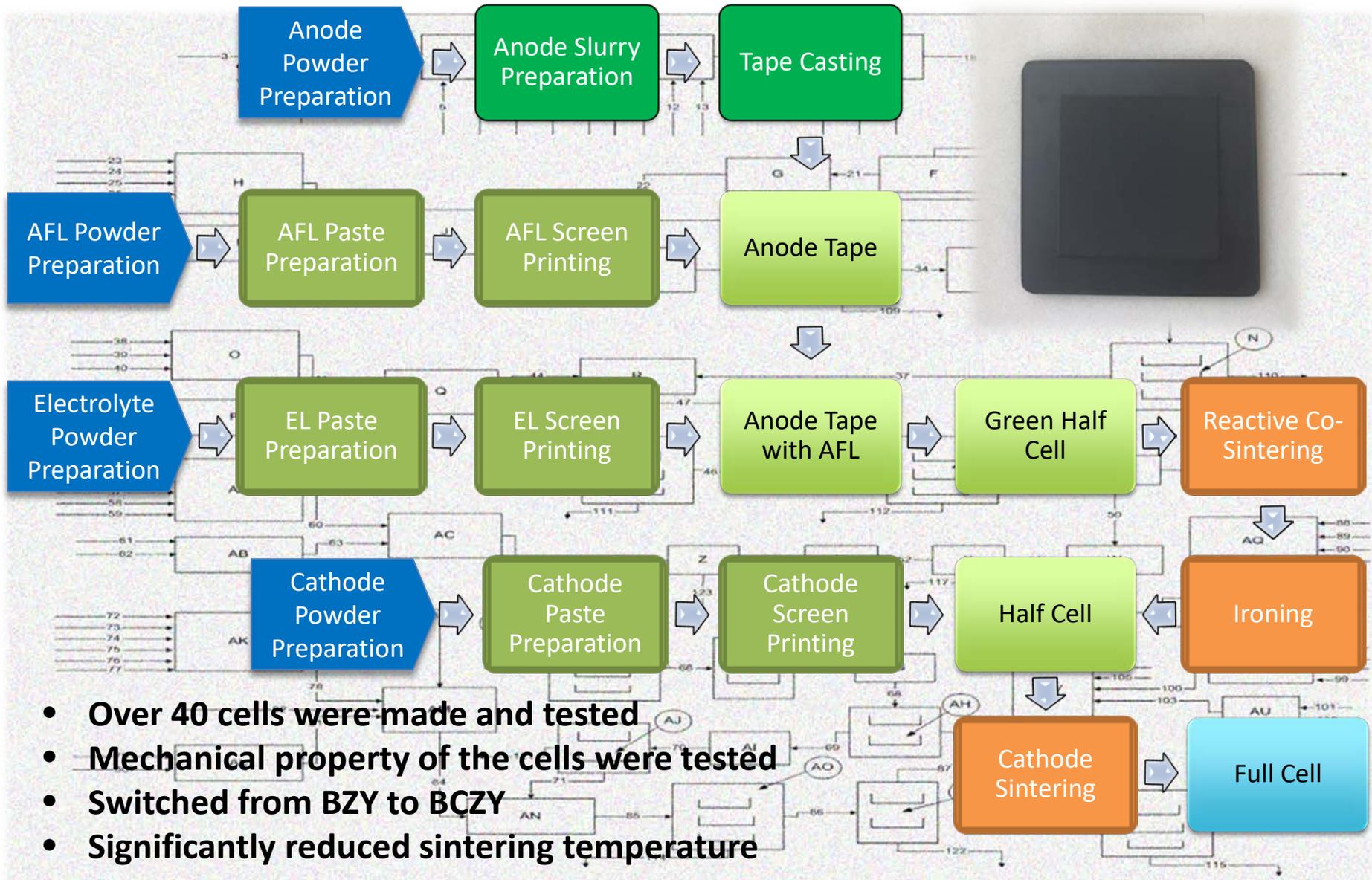


- Work was initiated to identify key degradation issues by testing in symmetric cells
- Project's First Quarter (Q1) Milestone was achieved by completing tests of H₂ & steam electrodes over 1000 hours
- Q3 Milestone was completed ahead of time by showing Faradaic efficiency > 85% and electric efficiency > 75% at 1 A / cm² in testing of button cells
- Development of cell area scale up and manufacturing process was initiated
- Activities related to the stack components and design were begun

TECHNICAL BACK-UP SLIDES

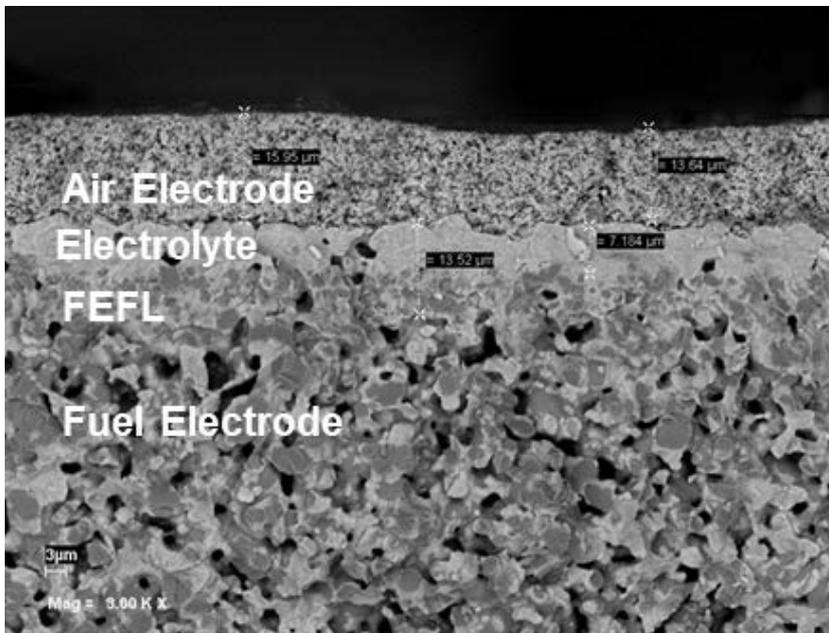
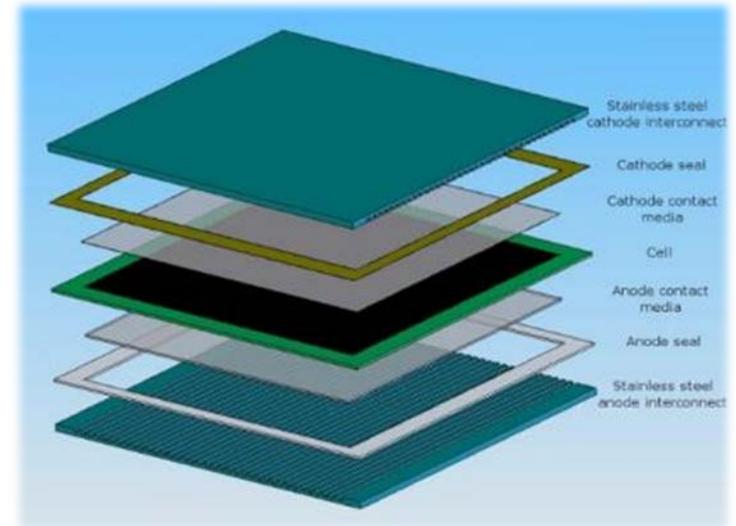


These processes are flexible & scalable to high volume and low cost production



- Over 40 cells were made and tested
- Mechanical property of the cells were tested
- Switched from BZY to BCZY
- Significantly reduced sintering temperature

- Fuel electrode-supported cell
- 0.5 to 1.5 mm fuel electrode (BCZYYb4411/Ni)
- ~15 micron fuel electrode functional layer (BCZYYb4411/Ni)
- ~10 micron electrolyte (BCZYYb4411)
- 10 - 50 micron air electrode
- 16 to 81 cm² active area

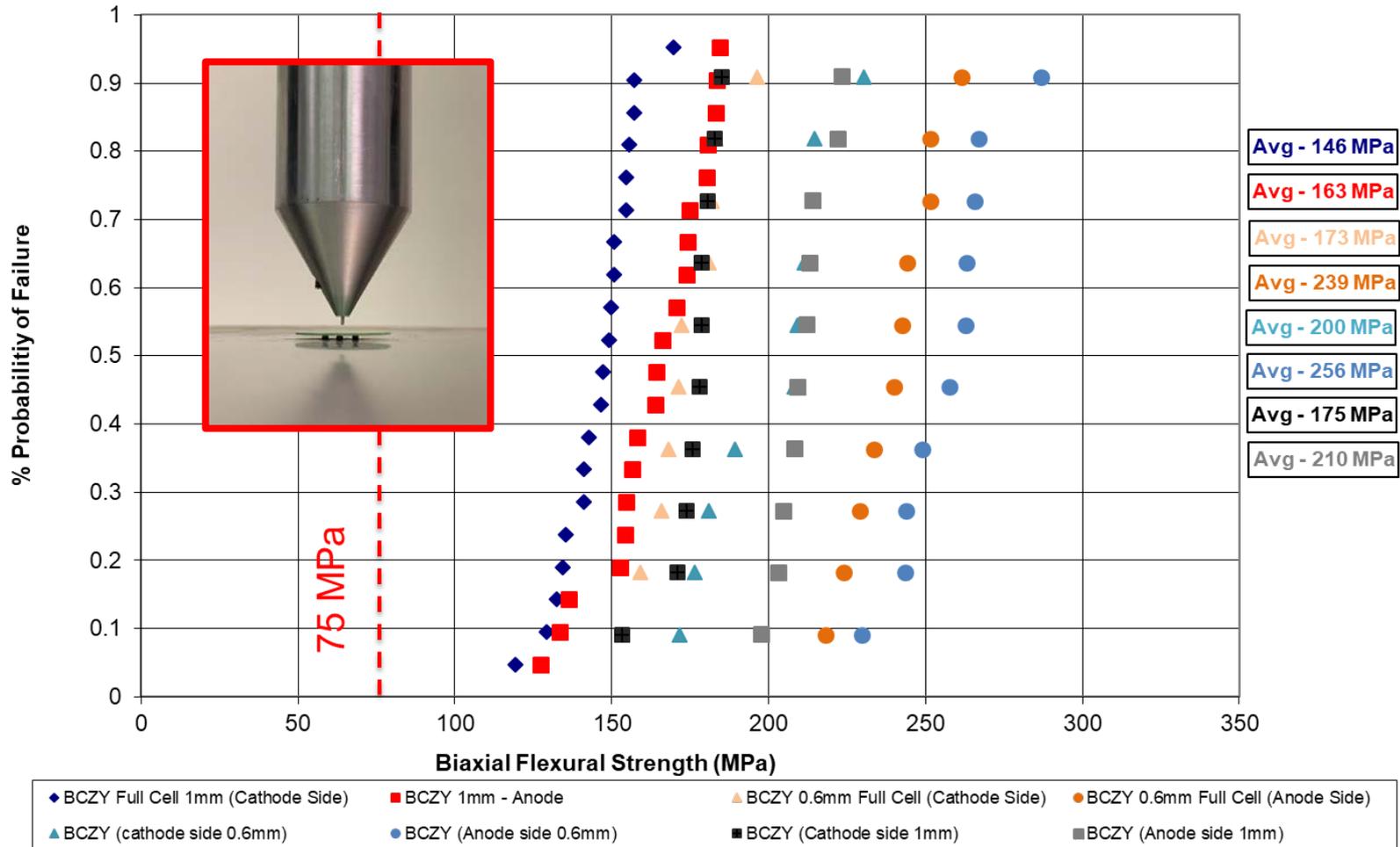


- Cell testing uses same materials and interfaces found in a stack repeat unit
- Cross-flow geometry
- Ferritic stainless steel current collection
- Seal and contact materials same as stack



Test results have shown that BCZY based cells have biaxial flexural strength higher than the targeted 75 MPa value

Failure Probabilities of Proton Conducting Cells



Excellent performance has been achieved by the proton conducting fuel cells in the temperature range of 500-600°C

